Preparation and Characterization of Nano Structured Pt-MOx/C for Oxygen Reduction Reaction in Acidic Medium

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**Introduction**

Oxygen reduction reaction (ORR) is one of the most important electrocatalytic reactions because of its role in corrosion of metals and electrochemical energy conversion especially in the field of fuel cells applications [1]. The cell voltage values of fuel cells are limited due to the slowness of ORR at the cathode. The most used electrocatalyst for ORR is platinum which is highly active chemically stable, but Pt is expensive and limited in the world’s supply; this results in difficulty of widespread commercialization of the fuel cell technology. So, research efforts in the development of cathode electrocatalysts have been focused on reducing the Pt content or replacing it with less expensive materials with maintaining high ORR activity [2], so getting electrocatalysts in which transition metals have been alloyed with noble metals is a need [3-5].

The principal problems that inhibit direct methanol fuel cells (DMFCs) commercialization are: development of a highly active and CO-tolerant anode catalysts and the overcoming of the oxygen reduction reaction (ORR) slowness at the cathode [6]. Considering that Pt catalysts alone we face a problem of the slowness of ORR which is due to the formation of - OH species at +0.8 V that inhibits further reduction of oxygen and hence results in loss of performance [7]. So, composite Pt-based electrocatalysts containing rare earth oxides have shown a number of characteristics that make them promising for catalytic studies due to the harmonic electronic effect in combining metal oxides, carbon and Pt. Strong d-d-Metal-Support Interaction of hyper-d-electronic metal with mostly hypo-d-oxide (TiO 2, ZrO 2, HfO 2) implies that the d-d-metal-oxide interaction is in accordance with the bonding strength which results in weakening of intermediate chemisorptive bonds (M-H, M-CO) [8-12]. Among the studied metal oxides, CeO 2 is predominant in the applications as catalyst support [13-17]. CeO 2 is a fluorite oxide whose cations can switch between +3 and +4 oxidation states, here the oxide acts as an oxygen buffer...
to control oxygen concentration at the catalyst surface. This may be due to the enhancement of the interaction between Pt and ceria for the catalytic activities of Pt [18, 19]. Cerium oxide nanoparticles were in-situ grown on reduced graphene oxide (rGO) through thermal treatment of the CeO₂-doped graphene oxide (GO) under nitrogen atmosphere. The nano composites show electrocatalytic activity toward the oxygen reduction reaction (ORR) in alkaline solution. Especially, the cerium oxide nanoparticles/rGO nanocomposites treated at 750 °C possess excellent electrocatalytic ability with a dominating four-electron pathway [20].

TiO₂ is promising because of its good electrochemical properties, chemical stability and non-toxic nature [21]. Pt-TiO₂/C shows improved stability in polymer electrolyte membrane fuel cells (PEMFCs) compared with Pt/C [22]. In spite of the amount of titanium dioxide and the crystalline phase (TiO₂, anatase/rutile phase) it was found that, it modifies the strength of the interaction between the substrate and the metal nanoparticles [23, 24]. The good effect of addition TiO₂ may be attributed to two factors which are: the changes in the Pt-d electronic properties and the geometric effect that leads to the Pt-Pt bonding distance contraction and hence results in a sensible improvement of the electrochemical reactions [25, 26]. Titanium oxide-based cathode, synthesized from oxy-titanium tetra-pyrazinoporphyrazine by the oxidation under a low partial pressure of oxygen using carbon nanotubes as a support, showed high reactivity in the four-electron reduction of oxygen [27]. Platinum nanoparticles (Pt NPs) have been anchored by photo deposition on titanium oxide (TiO₂) matrix which is formed via titanium isopropoxide hydrolysis on cup-stacked carbon nanotubes (CSCNT) in isopropanol, the resultant composite Pt catalyst was tested for oxygen reduction reaction (ORR) in acidic media and the results revealed that the anchoring of Pt NPs on the TiO₂ support material deposited on CSCNT is an effective way to enhance the ORR activity of Pt NPs [28]. A 15 wt.% Pt-based catalyst was developed on a mixture of titanium suboxides, with an excess of the TiO05 phase, doped with Mo, as a TiO₂-Mo without carbon support and compared to a commercial 20 wt.% Pt/C (E-TEK). The Pt/TiO₂-Mo catalyst shows an excellent electroactivity and stability toward the ORR, reaching a performance of 73.3 mA mg⁻¹, nearly twice as that of the commercial Pt/C, with a current density of 1.1 mA cm⁻² at 0.9 V vs RHE, and an half-wave potential of 0.86 V vs RHE [29]. Pt/ZrO₂@CNx has been synthesized by forming a highly conductive nitrogen-doped carbon layer on the surface of ZrO₂ (ZrO₂@CNx) the final step is the Pt nanoparticles deposition. The Pt/ZrO₂@CNx catalyst showed a high electrocatalytic activity for the oxygen reduction reaction (ORR) [30]. A two-step method has been used by G. Liu et al. to prepare Pt/ZrO₂/C catalyst as a cathode catalyst in a high temperature PEMFC based on H₃PO₄ doped polybenzimidazole (PBI) to investigate the cell performance [31]. Cobalt oxide (Co₃O₄) nanocubes were incorporated into reduced graphene oxide (RGO) using a simple single-step hydrothermal reaction for an electrocatalytic oxygen reduction reaction (ORR). The RGO@Co₃O₄ nano hybrid with 4 wt% of graphene oxide modified glassy carbon (GC) electrode exhibited better electrocatalytic activity when compared to the other controlled modified electrodes and commercial Pt/C catalyst for the ORR in an alkaline medium [32]. Bifunctional electrocatalysts series composed of nitrogen-doped graphene cobalt oxide nanoparticles nano-hybrids (Co-N/G) are fabricated through one-pot hydrothermal synthesis, The optimized Co-N/G catalyst consists of the highest contents of pyridinic nitrogen and CoO, efficiently catalyze both ORR and OER [33].

Microwave-assisted technology has been widely used for preparing many nanomaterials because it is a quick, simple, homogeneous and efficient method [34-36]. Smaller particles were formed when microwave irradiation method was adopted. It was reported that Pt particles with about 3-4 nm size exhibited a higher mass electrocatalytic activity for oxygen reduction [37, 38]. Pt-Ru particles with 3 nm size displayed the highest mass catalytic activity for methanol electrooxidation [39]. So as a direct result, microwave irradiation method is applicable in different areas namely; materials synthesis, food drying, microwave-induced catalysis and plasma chemistry [40-43].

The present work aims to study physical and electrochemical behavior of Pt-MOx/C electrocatalysts, where MOx refers to TiO₂, CeO₂ and ZrO₂ in order to develop a cheaper and more efficient electrocatalyst for oxygen reduction reaction. Pt/C has been studied to evaluate the metal oxide effect; Pt-CeO₂/C-1 has been studied to evaluate the effect of the changing of the used reducing agent on the behavior of the prepared electrocatalyst.

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Experimental

Catalyst synthesis

All the reagents in this synthesis were in analytical grade (Sigma-Aldrich) and used without further purification. Double distilled water was used in all aqueous solutions preparation and washing. According to this preparation method, we have synthesized Pt-TiO₂/C, Pt-CeO₂/C and Pt-ZrO₂/C electrocatalysts using titanium (IV) oxide (TiO₂), cerium (IV) oxide (CeO₂) and zirconium (IV) oxide (ZrO₂), respectively through two steps. The first step involved the synthesis of MOₓ/C powders via solid state reaction under intermittent microwave heating, while the second step is platinum loading on MOₓ/C surfaces. To prepare MOₓ/C, a fixed amount of titanium (IV) oxide (TiO₂), cerium (IV) oxide (CeO₂) or zirconium (IV) oxide (ZrO₂) [5 wt.%] well dispersed over carbon black Vulcan XC−72R using a mixture of second distilled water and isopropanol in the ratio of 1:1. This suspension was stirred using magnetic stirrer for 30 min and heated into a microwave oven (Caira CA-MW1025, touch pad digital control, 50 MHz, 1400 W) in six cycles; each cycle was 20 s on and 60 s off. The next step is the filtration of the mixture and washing it with double distilled water for 6 times, the last step is drying in an air oven at 80°C for 6 h. Reduction of platinum on the prepared MOₓ/C powders is done through modified microwave-assisted polyl process in which H₂PtCl₆ solution was added to a suspension of MOₓ/C powder in distilled water with adjusting Pt loading at 25 wt.%. For this step, a mixture of ethylene glycol and sodiumborohydride (EG + NaBH₄) were used (in this case the electrocatalysts are assigned as Pt-MOₓ/C). pH of the solution was adjusted at 10 using 0.4 M KOH in ethylene glycol to induce the formation of small and uniform Pt nanoparticles. This mixture was then heated into the microwave oven for 50 s in one continuous mode. Pt-MOₓ/C powder was then filtered, washed and dried. Pt-CeO₂/C-1 was prepared via the same procedure using single reducing agent ethylene glycol (EG) for studying the effect of changing the reducing agent during the preparation process.

Physical characterization

XRD, TEM and EDX analyses are used to describe Pt/C and the mentioned Pt-MOₓ/C electrocatalysts physically. Specifications of devices used to evaluate these types of analyses are: a RigakuD/MAX-PC 2500 X-ray diffractometer equipped with Ni filtered Cu Ka as the radiation source. The tube current was 40 mA with a voltage of 40 kV to evaluate the crystalline structure of the prepared electrocatalysts. TEM and EDX analyses was performed using JEOL-JEM 2010 transmission electron microscope that operated at an accelerating voltage of 160 kV.

Electrochemical measurements

Voltamaster 6 potentiostat and Rotating Disc Electrode (RDE) were employed for the electrochemical measurements. It is connected to a personal computer as data interface. Cyclic voltammetry (CV) and linear sweep voltammetry (LSV) were conducted to measure the electrocatalytic activity of the prepared Pt–MOₓ/C electrocatalysts towards oxygen reduction reaction. The three electrode cell consists of Pt wire and Ag/AgCl as the counter and the reference electrodes, respectively. All the potential values in this work are referred to RHE. The working electrode was a thin film of electrocatalyst supported on glassy carbon (GC) electrode (with geometrical surface area of 0.196 cm²) which is a part of the RDE. This GC electrode was first polished using 0.05 μm alumina powder and soft cloth then carbon-supported electrocatalyst was put on it mixed with 1 droplet of isopropanol, two consecutive droplets of 5% Nafion solution were put after isopropanol has dried, at last a second droplet of isopropanol was added, the electrocatalyst thin film was left till air drying. The catalyst loading is 0.6 mg/cm².

For the electrochemical active surface area (ECSA) determination experiments, they were carried out at room temperature employing 0.5 M H₂SO₄ as the electrolyte solution and three electrode system in which Hg/Hg₂SO₄/1.0 M H₂SO₄(MMS) is the reference electrode. Thirty CVs with scan rate of 50 mVs⁻¹ at a potential window (-700 to 900 mV/MMS) (-80 to 1520 mV/RHE) was conducted.

All electrochemical experiments were carried out at room temperature and ambient pressure employing 0.5 M H₂SO₄ as the electrolyte solution. At first nitrogen was bubbled for 20 min. The CV scan at the 10th cycle is recorded scan rate of 50 mVs⁻¹ with a potential window (-200 to 1000 mV/Ag/AgCl) (-1 to 1199 mV/RHE) and one LSV with scan rate of 10 mVs⁻¹ in a potential range (1000 to-200 mV/Ag/AgCl) (1199 to-1 mV/RHE) was performed, then oxygen bubbling for 30 min, after that LSVs with different rpm values ranging between 200 rpm to 2400 rpm were performed in solution saturated with...
oxygen with the same conditions as in case of LSV performed in solution saturated with nitrogen. The same conditions of CV recorded in nitrogen is repeated in case of oxygen.

Results and Discussion

Physical characterization of Pt-MOx/C electrocatalysts

Figure (1a) showed the X-ray diffraction (XRD) of Pt-TiO$_2$/C, Pt-CeO$_2$/C and Pt-ZrO$_2$/C electrocatalysts in comparison with that of Pt/C. The diffraction peaks of Pt(111), Pt(200) and Pt(220) appear in allelectrocatalysts. XRD pattern of Pt-CeO$_2$/C-electrocatalysts shows that CeO$_2$ has four diffraction peaks of CeO$_2$ at $2\theta = 28.6^\circ$, $33.1^\circ$, $47.5^\circ$ and $56.3^\circ$ that correspond to (111), (200), (220) and (311) diffraction planes, respectively[44].These are typical of single-phase oxides with fluorite structures. so, both Pt and CeO$_2$ phases exist simultaneously in Pt-CeO$_2$/C electrocatalyst, it was also noticed that; after introducing CeO$_2$ to Pt/C in Pt-CeO$_2$/C electrocatalyst, 20 values are shifted in the positive direction when compared to those of Pt in Pt/C as shown in Table 1 while for Pt-ZrO$_2$/C electrocatalyst Pt(111), Pt(200) and Pt(220) planes are observed at $2\theta = 39.765^\circ$, $45.909^\circ$ and $67.682^\circ$, respectively.

Pt(111) and Pt(220) planes are shifted to higher 20 values when compared to those of Pt/C as shown in Table 1. This is an indication for the fact that incorporation of ZrO$_2$ affects the crystalline lattice of platinum; no diffraction planes related to ZrO$_2$ phase were found. This can be due to the low concentration of ZrO$_2$ or partial ZrO$_2$ entering into Pt crystalline lattice[45-48]. For Pt-TiO$_2$/C electrocatalyst we can notice that; Pt(111) Pt (200) and Pt(220) diffraction planes are found to be at higher 20 values when compared to those in Pt/C as in Table 1 resulting in a crystal lattice contraction, it is also noticed from Fig.1 (a) that; no characteristic peak for TiO$_2$ is found in XRD pattern, this could be interpreted by the existence of the titanium oxide in an amorphous form[49]. Pt (200) diffraction planes of Pt-CeO$_2$/C-1, showed 20 shift to higher values 47.326 when compared to that of Pt-CeO$_2$/C47.319 as seen from Fig.1b while the corresponding interplanar spacing parameter is constant 1.919. Pt (111) and Pt (220) diffraction planes of Pt-CeO$_2$/C-1 show no values, so we can conclude that introducing CeO$_2$ in Pt-

![Fig.1. XRD patterns of (a) Pt/C and different Pt–MOx/C electrocatalysts, (b) Pt–CeO$_2$/C and Pt–CeO$_2$/C-1 electrocatalysts.](image)

<table>
<thead>
<tr>
<th>Electro catalyst</th>
<th>Pt(111)</th>
<th>Pt(200)</th>
<th>Pt(220)</th>
<th>Pt Crystallite size / nm</th>
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<td>20 / Å</td>
<td>d / Å</td>
<td>20 / Å</td>
<td>d / Å</td>
</tr>
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<td>Pt/C</td>
<td>39.265</td>
<td>2.293</td>
<td>46.001</td>
<td>1.971</td>
</tr>
<tr>
<td>Pt–TiO$_2$/C</td>
<td>39.678</td>
<td>2.270</td>
<td>46.339</td>
<td>1.958</td>
</tr>
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<td>2.272</td>
<td>47.319</td>
<td>1.919</td>
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<td>2.264</td>
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<tr>
<td>Pt–CeO$_2$/C-1</td>
<td>-</td>
<td>-</td>
<td>47.326</td>
<td>1.919</td>
</tr>
</tbody>
</table>

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CeO\(_2\)/C-1 leads to crystal lattice contraction. It was found that the Pt particle size for Pt in Pt-CeO\(_2\)/C is 3.2 nm while that in Pt-ZrO\(_2\)/C, Pt-TiO\(_2\)/C and Pt-CeO\(_2\)/C-1 electrocatalysts could not be estimated, this phenomena is attributed to the fact that, XRD gives information about crystalline size information rather than true particle size\[50\].

Energy dispersive X-ray (EDX) analysis has been carried out to determine the elemental composition of the prepared Pt/C and Pt-MO\(_x\)/C electrocatalysts. Figure 2 (a-e) present the (EDX) spectra of Pt/C, Pt-TiO\(_2\)/C and Pt-CeO\(_2\)/C, Pt-ZrO\(_2\)/C and Pt-CeO\(_2\)/C-1 electrocatalysts respectively. The weight and atomic percentages of different elements constituting these electrocatalysts are presented in Table 2. Wt. % of Pt was found to be 36.03 in Pt/C electrocatalyst. This percentage was increased when different MO\(_x\) were introduced. All studied samples found to contain carbon, oxygen and platinum in different weight percentages. It is noticed from Table 2 that Pt-ZrO\(_2\)/C electrocatalyst showed the highest weight percentages of Pt (56.03) while Pt-CeO\(_2\)/C-1 electrocatalyst showed the lowest one (10.39). On the other hand we found that; Pt-CeO\(_2\)/C has the highest weight percentage value for the metal (here; Ce) 8.84.

On studying the effect of reducing agent we can observe that, using single reducing agent (EG) decreases the Wt.% of Pt and M (Ce) while increases that of C and O. It was also noticed that the weight percentage of oxygen for electrocatalysts prepared using mixed reducing agent is low when compared to that prepared using single reducing agent.

Transmission electron microscopy (TEM) image of Pt/C electrocatalyst was shown in Fig.
A higher degree of particle agglomeration is observed with particle size of 3.57 nm as shown in Table 3. Figure (3b& 3b') display TEM images of Pt–TiO$_2$/C electrocatalyst. The catalyst particles were homogeneously dispersed on the carbon support in with Pt particle size of 3.06 nm. (Fig.3c&3c') Figure(3e& 3e') show TEM images of Pt–CeO$_2$/C and Pt–CeO$_2$/C-1, respectively. The addition of CeO$_2$ to Pt/C using a single reducing agent of (EG)during the reduction step decreases the resultant Pt particle size (2.50 nm) while using mixed reducing agent (EG +NaBH$_4$) increases Pt particle size (2.78 nm) which in agreement with the fact that; the used reducing agent strongly affects morphology and ORR activity of nano carbon supported electrocatalysts. Using different reducing agents, namely; ethylene glycol (EG), borohydride (NaBH$_4$) and formaldehyde (HCHO) resulted in producing electrocatalysts with different particle size. The method with (EG) has resulted in the smallest mean particle sizes in the range between 4.6 and 6.6 nm, the electrocatalyst based on NaBH$_4$ provided the mean particle size ranging between 4.6 and 13.3 nm, while that based on HCHO has showed a mean particle size in the range 8.8 - 22.9 nm[51].When CeO2 is added to Pt/C in Pt–CeO$_2$/C electrocatalyst as in Figs. 3c,c' aggregated particles are shown, this could be attributed to the tendency of Pt-CeO$_2$ nanoparticles to form agglomerates[52]. TEM images of Pt–ZrO$_2$/C electrocatalyst represented in Figs. (3d&3d') Pt particle size was found to be 3.49 nm which is little bit smaller than that of Pt/C (3.57 nm), this is somewhat similar to results obtained by Liu et al. who found that; The particle size for Pt/C catalyst is 3.0 nm while that of Pt$^4$ZrO$_2$/C catalyst is 4.2 nm(31).

Electrochemical characterization

Electrochemical surface area (ECSA) evaluation

The electrochemical active surface area

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The ECSA (m²g⁻¹) of a catalyst is calculated according to the following equation [53, 54]:

\[
\text{ECSA (m}^2\text{g}^{-1}) = \frac{Q_H}{[\text{Pt}]} \quad (1)
\]

where \(Q_H\) (C m⁻²) is the charge of hydrogen desorption, \([\text{Pt}]\) (g m⁻²) is the quantity of Pt loading on the electrode.

ECSA of the prepared electrocatalysts was estimated by integrating the voltammograms corresponding to hydrogen adsorption–desorption area. It is so obvious from Fig.4 that all Pt-Mo/C have higher ECSA values than that of Pt/C as shown in Table 4 which is could be due to the presence of more active sites on the Pt-Mo/C surfaces than those on Pt/C surface [55].

Pt-ZrO₂/C and Pt-CeO₂/C electrocatalyst has the highest ECSA value among all studied electrocatalysts which are 69.60 and 46.93 m²g⁻¹ respectively, but in case of Pt-TiO₂/C, it was noticed that; although its mass activity at 0.65V/RHE is -0.567 mAmg⁻¹ which is smaller than that of Pt/C that equals-2.11mAmg⁻¹, it was found to have higher ECSA value, 32.90 m²g⁻¹ than that of Pt/C which is 24.60 m²g⁻¹, this could be attributed to the smaller Pt size of Pt-TiO₂/C (3.06 nm) in comparison with Pt/C (3.57 nm) and better Pt dispersion as seen in Fig.(3a, 3a' and 3 b, 3b'). This is in accordance with Gustavsson et al. who showed that the presence of TiO₂ can either increase or decrease the ORR performance of Pt catalyst, depending on the sequence through which the thin films have been deposited which comes in accordance with the fact that; synthesis method has been found to make changes in the Pt electronic and geometric parameters [40].

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On comparing the two prepared Pt-CeO$_2$/C; namely: Pt-CeO$_2$/C and Pt-CeO$_2$/C-1 we noticed that, changing the used reducing agent affects the behavior of the resultant electrocatalyst, as calculated from Equation 1, Pt-CeO$_2$/C showed higher ECSA value that equals 46.93 m$^2$g$^{-1}$ than that of Pt-CeO$_2$/C-1; 39.85 m$^2$g$^{-1}$. Another observation is related to both Pt-ZrO$_2$ carbon supported electrocatalyst which is although it has large particle size (3.49 nm) it showed the highest ECSA and electrocatalytic activity, this could be explained by the fact that the difference in particle size is not huge to the extent that affects its catalytic activity if compared to results obtained by Oishi and Savadogo who synthesized Pd electro-catalyst monolayer on different single crystal substrates which was found to have wide range of particle sizes up to 92 nm with mean value of 18–20 nm[56].

**Cyclic voltammetry results**

Cyclic Voltammograms curves (CVs) in oxygen saturated solution were recorded in the potential range from -1.0 to 1199 mV/RHE. The results of Pt/C and Pt-MOx/C catalysts are presented in Fig. 5, the voltammograms shape is the typical shape of that of Pt nanoparticles in acid medium[57, 58]. Pt/C, Pt-TiO$_2$/C and Pt-CeO$_2$/C electrocatalysts show:

- The characteristic H adsorption- desorption peak at 0.05-0.3 V/RHE while that for Pt-ZrO$_2$/C lies at 0.05-0.4 V/RHE.
- Pt oxide formation-reduction peaks at 0.85/0.60 V/RHE.
- It could be easily noticing that; Pt-ZrO$_2$/C and Pt-CeO$_2$/C have the highest Pt oxidation-reduction peaks among the prepared electrocatalysts.

**Study of oxygen reduction with RDE**

Figure represents linear sweep voltammograms (LSVs) of Pt/C and Pt-MOx/C where (M = Ti, Ce or Zr), it is obvious that, all prepared Pt-MOx/C electrocatalysts have higher activity towards ORR than Pt/C except for Pt-TiO$_2$/C. Moreover Pt-ZrO$_2$/Chas the highest mass activity values at 0.65V/RHE that equals -9.75 mAmg$^{-1}$. i.e. the best activity towards ORR when it was compared with the other catalysts, this is because ZrO$_2$ was found to have fairly high oxygen storage capacity, which enlarges the oxygen concentration at the catalyst surface, and achieves higher ORR activity with maintaining the catalyst at the same oxygen pressure[59].

Regarding forPt-CeO$_2$/C; it has high activity for ORR as seen from Fig. 6 and shows a good catalytic activity for ORR; -2.240 mAmcm$^{-2}$ at...
0.65V/RHE which is higher than that of Pt/C(-1.262mAcm$^{-2}$) at the same potential value as seen in Table 4, this could be interpreted in the light of the fact that, Pt-CeO$_x$ appears to have a characteristic system when compared to other Pt-oxide composite catalysts; the active oxygen supplied from CeO$_2$ to Pt surface contributed to the improvement of the ORR activity of the Pt-CeO$_x$ cathode, so this noticed behaviour of high ORR activity of Pt-CeO$_x$/C may be improved by formation of Pt surface partially covered by amorphous Ce$_2$O$_3$ layer or may be due to the role of ceria layer in Pt oxide formation on Pt[60].

On evaluating the performance of mentioned electrocatalysts prepared using the mixed reducing agent, it was found that Pt–CeO$_2$/C has a higher potential value; 1097.9 mV/RHE than that of Pt-TiO$_2$/C; 967.9 mV/RHE at zero current, this big difference which equals 130.0 mV is related to the difference in mass activity value at 0.65V/RHE which is -2.240 mAcm$^{-2}$ for Pt-CeO$_2$/C and -0.340 mAcm$^{-2}$ for Pt-TiO$_2$/C, meaning that increasing in the mass activity value of Pt–CeO$_2$/C 6.588 times as that of Pt-TiO$_2$/C. The case is different for Pt–ZrO$_2$/C in which the mass activity value at 0.65V/RHE is the highest among the studied Pt-MOx/C; -5.840 mAcm$^{-2}$. The onset potential is known as the potential at which the current for oxygen reduction is first observed[61]. Here the onset potential value for Pt–ZrO$_2$/C is the highest one among the studied electrocatalysts; 1041.2 mV/RHE indicating that the oxygen reduction catalytic activity of this electrocatalyst exceeds the other catalysts regarding to onset potential values; the higher onset potential values the higher catalytic activity towards ORR[62] as seen from Fig 6.

Figure 7 (a, b) shows the (LSVs) of ORR on the Pt-CeO$_2$/C and Pt-CeO$_2$/C-1 electrodes respectively in O$_2$ saturated 0.5 M H$_2$SO$_4$ solution with rotation rates ranging between 200-2400 rpm.

Clear performance differences between the two catalysts can be figured out by comparing the LSVs of a particular electrode rotation speed. It is very clear that there is an extrusive relation between cathodic current values and the rate of electrode rotation. The studied catalyst samples show the same ORR open circuit potential (around 1040 mV for Pt-CeO$_2$/C-1 and around 1080 mV for Pt-CeO$_2$/C), generally this is in consistent with the expected behavior for ORR in aqueous acid medium catalyzed by Pt nanoparticles on carbon supports[60].

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The increase in the diffusion limiting current in the RDE measurement is directly proportional to the rotation speed. The limiting current densities of Pt-CeO$_2$/C increased from 1.25 to 1.80 mA cm$^{-2}$ while that of Pt-CeO$_2$/C-1 increased from 0.82 to 1.55 mA cm$^{-2}$ as the rotation speeds were increased from 200 to 2400 rpm, this behavior could be explained by the fact that; higher rotation speeds leads to faster oxygen flux at the electrode surface and hence generating higher currents.

Hydrated oxide reduction produced by applying a reducing agent. Typical reducing agents are H$_2$ where strength of reduction is controlled by temperature and NaBH$_4$ which have strong reduction strength at room temperature.

Comparing Pt-CeO$_2$/C and Pt-CeO$_2$/C-1 in Fig. (7a, 7b) we can easily notice that, for 2400 rpm, Pt-CeO$_2$/C had a higher current density value at 0.65V/RHE; -2.240 mA cm$^{-2}$ than that of Pt-CeO$_2$/C-1 that equals to -1.597 mA cm$^{-2}$, this could be related to the fact that, smaller particle sized electrocatalysts produced from using single reducing agent may tend to agglomerate and hence reduce the activity of the whole electrocatalysts, hence the oxide reduction extent in the preparation method affects the Pd and Au performance towards the ORR which is related to the catalyst synthesis procedures.

From the comparison of the LSVs recorded for both Pt-CeO2 on Carbon catalysts at 2400 rpm we can easily also observe the differences in the open circuit potential, limiting current and half wave potential values. The open circuit potential is higher in case of Pt-CeO$_2$/C catalyst; 1097.9 mV/RHE than in case of Pt-CeO$_2$/C-1; -1055.3 mV/RHE, faster ORR is observed in the whole potential window for Pt-CeO$_2$/C than on Pt-CeO$_2$/C-1 catalyst. The half wave potential of Pt-CeO$_2$/C was shifted to about 100 mV in the positive side compared to Pt-CeO$_2$/C-1. Similarly, the limiting current of Pt-CeO$_2$/C catalyst is higher by about 300 mA (regardless to the sign) compared to Pt-CeO$_2$/C-1. The favorable shifts in the open circuit, half wave potential and limiting current regions equivalent to the electrode of Pt-CeO$_2$/C can be attributed to the enhanced ORR activity. It was found that the difference in the limiting currents for the two electrocatalysts may

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**Table 2. Weight and atomic percentages of different elements forming Pt/C and different Pt-MO$_x$/C electrocatalysts**

<table>
<thead>
<tr>
<th>Element</th>
<th>Pt/C</th>
<th>Pt-TiO$_2$/C</th>
<th>Pt-CeO$_2$/C</th>
<th>Pt-ZrO$_2$/C</th>
<th>Pt-CeO$_2$/C-1</th>
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<tbody>
<tr>
<td>C</td>
<td>63.97</td>
<td>42.82</td>
<td>44.40</td>
<td>44.60</td>
<td>37.69</td>
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<tr>
<td>O</td>
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<td>4.54</td>
<td>6.10</td>
<td>4.49</td>
<td>5.60</td>
</tr>
<tr>
<td>Ce</td>
<td>-</td>
<td>2.27</td>
<td>4.80</td>
<td>6.40</td>
<td>10.39</td>
</tr>
<tr>
<td>Zr</td>
<td>-</td>
<td>5.24</td>
<td>2.80</td>
<td>0.68</td>
<td>0.79</td>
</tr>
</tbody>
</table>

**Table 3. Particle size values of Pt/C and different Pt-MO$_x$/C electrocatalysts according to TEM analysis.**

<table>
<thead>
<tr>
<th>Electrocatalyst</th>
<th>Particle size / nm</th>
</tr>
</thead>
<tbody>
<tr>
<td>Pt/C</td>
<td>3.57</td>
</tr>
<tr>
<td>Pt-TiO$_2$/C</td>
<td>3.06</td>
</tr>
<tr>
<td>Pt-CeO$_2$/C</td>
<td>2.78</td>
</tr>
<tr>
<td>Pt-ZrO$_2$/C</td>
<td>3.49</td>
</tr>
<tr>
<td>Pt-CeO$_2$/C-1</td>
<td>2.50</td>
</tr>
</tbody>
</table>

**Table 4. Electrochemical parameters and electrochemical surface area values obtained from LSVs and CVs of Pt/C and Pt-MO$_x$/C electrocatalysts 0.5 MH$_2$SO$_4$ solution.**

<table>
<thead>
<tr>
<th>Electrocatalysts</th>
<th>Open circuit pot. [mV/RHE] at 0 current</th>
<th>Onset ORR [mV/RHE]</th>
<th>ECSA [m$^2$ g$^{-1}$]</th>
<th>Current density at 650 mV/RHE</th>
</tr>
</thead>
<tbody>
<tr>
<td>Pt/C</td>
<td>899.5</td>
<td>830.1</td>
<td>24.60</td>
<td>-1.262</td>
</tr>
<tr>
<td>Pt-TiO$_2$/C</td>
<td>967.9</td>
<td>790.5</td>
<td>32.90</td>
<td>-0.34</td>
</tr>
<tr>
<td>Pt-CeO$_2$/C</td>
<td>1097.9</td>
<td>931.4</td>
<td>46.93</td>
<td>-2.240</td>
</tr>
<tr>
<td>Pt-ZrO$_2$/C</td>
<td>801.0</td>
<td>1041.2</td>
<td>69.60</td>
<td>-5.840</td>
</tr>
</tbody>
</table>

(86x785) Egypt. J. Chem. 60, No.3 (2017)
be due to the difference of oxygen diffusion at both of them[72]. It is also found that Pt-CeO$_2$/C (8.84 Ce%) had higher onset potential and limiting current than Pt-CeO$_2$/C-1 (6.40 Ce%) which is in accordance with Kang et al.[73]

Oxygen reduction mechanism of Pt-CeO$_2$/C and Pt-CeO$_2$/C-1 has been evaluated using the Koutecky-Levicheq equation to determine the number of electrons transferred per O$_2$ molecule.

\[
\frac{1}{I} = \frac{1}{I_k} + \frac{1}{0.62 n F A D^{1/2} c_{O_2}^{1/2} \omega^{1/2}}
\]

(2)

where $I_k$ is the kinetic current; $\omega$ is the rotation rate; $n$ is the number of electrons involved in the reaction; $F$ is Faraday constant; $A$ is the geometric area of the disk electrode; $D$ and $c$ are the diffusion coefficient of dissolved oxygen and the concentration of dissolved oxygen in 0.5M H$_2$SO$_4$, respectively; $\nu$ is the kinematic viscosity of the electrolyte.

Figure 8 a, b represents Koutecky-Levich (-1/I versus $\omega^{-1/2}$) plots for the ORR on Pt-CeO$_2$/C and Pt-CeO$_2$/C-1 electrodes respectively at electrode potential range from 0.2V - 0.5V vs. RHE in 0.5M H$_2$SO$_4$. The linearity and the parallism of these plots indicate first-order kinetics with respect to molecular oxygen[74]. The calculation of $n$ was performed using the values: $F= 96,485$ Cmol$^{-1}$; $A = 0.196$ cm$^2$; $D = 1.93 \times 10^{-5}$ cm$^2$ s$^{-1}$; $c = 1.13 \times 10^{-6}$ mol cm$^{-3}$; $\nu = 9.5 \times 10^{-3}$ cm$^2$ s$^{-1}$[75]. Intercept different values at the y-axis indicate the existence of different kinetic constants at different electrode potentials while the non-zero values of the intercepts imply that the ORR is not controlled solely by diffusion [76].

Fig. 8. Koutecky-Levich plot drawn at different potentials for (a) Pt- CeO$_2$/C, b) Pt- CeO$_2$/C-1 in O$_2$-saturated 0.5 M sulphuric acid solution at 2400 rpm, scan rate 10 mVs$^{-1}$.

Conclusion

Pt-MO$_x$/C electrocatalysts have been prepared through two steps. The first step involves the synthesis of MO$_x$/C powders via solid state reaction under intermittent microwave heating, while the second step is platinum loading on MO$_x$/C surfaces using ethylene glycol or a mixture of ethylene glycol and sodium borohydride as the reducing agent.

- The preparation method of the electrocatalysts is found to affect their behaviour towards ORR.
- Pt-CeO$_2$/C and Pt-ZrO$_2$/C have the highest activity for oxygen reduction among the studied electrocatalysts and also higher than that of prepared Pt/C in acid medium.
- Changing the used reducing agent was found to affect the electrocatalytic efficiency and electrochemical surface area of the resultant electrocatalyst.
- Pt-CeO$_2$/C and Pt-CeO$_2$/C-1 showed first-order kinetics with respect to molecular oxygen with oxygen reduction reaction not controlled solely by diffusion.

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تحضير و توصيف تراكيب نانومترية من البلاتين و أكاسيد العناصر الانتقالية لتفاعلات اختزال الأكسجين في الأوساط الحامضية

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تم تحضير العوامل الحفازة المتكونة من البلاتين و أكاسيد بعض العناصر الانتقالية و المدعمة بالكربون لتطوير عامل حفاز رخيص و فعال لتفاعل اختزال الأكسجين باستخدام عامل مختزل ثنائي (بلاتين جليكول + بوروهيدريد الصوديوم) حيث أن العناصر الانتقالية المستخدمة هي البلاتين، السيريوم و الزيركونيوم. تم دراسة البلاتين المدعم بالكربون المكون من البلاتين و أكاسيد السيريوم و المحضر باستخدام البلاتين جليكول مكوناً لدراسة تأثير تغير العامل المختزل على شكل العامل الحفاز لتفاعل اختزال الأكسجين وكذلك حركة تفاعل اختزال الأكسجين. و قد تم تتبع النشاط الحافزي الكهربي للعامل الحفازة المحضرة لتفاعل اختزال الأكسجين باستخدام الفولتامترية الدائري و المسح الفولتامترى الكهروضوئي للعامل الحفازة المحضرة لتفاعل اختزال الأكسجين المكون من البلاتين و أكاسيد الزيركونيوم. وقد أظهر العامل الحفاز المكون من البلاتين و أكاسيد الزيركونيوم أفضل نشاط لتفاعل اختزال الأكسجين حيث وجد أن كثافة تيار اختزال الأكسجين له (40 م أمبير/س) حوالي خمسة أضعاف كثافة تيار اختزال الأكسجين عند استخدام البلاتين المدعم بالكربون (262 م أمبير/س). كما وجد أن العامل الحفاز المكون من البلاتين و أكاسيد السيريوم المحضر بعامل مختزل ثنائي له تأثير اختزال أكسجين أفضل (40 م أمبير/س) من العامل المكون من البلاتين و أكاسيد السيريوم المحضر بعامل مختزل الأحادي (159 م أمبير/س) مما يوضح التأثير الكبير لتفاوت العامل المختزل في نشاط العامل الحفازة الحاصلة لتفاعل اختزال الأكسجين. كماً أيضاً على حجم الجسيمات و سطح العناصر الانتقالية في العامل الحفازة. أظهرت دراسة حركة تفاعل اختزال الأكسجين للعامل الحفازة المتكون من البلاتين و أكاسيد السيريوم باستخدام معادلة كويكباتي و أظهرت أنه تفاعل من الدرجة الأولى. تم استخدام حبوب الأشعة السينية و الطاقة المتبددة للأشعة السينية وكذلك الميكروكنبيهكتروكفيت لتوسيع العوامل الحفازة المحضرة.