

Synthesis and Characterization of Ion Exchanger Based on Waste Cotton for Dye Removal from Wastewater

A.I. Waly¹, M.A. Khedr², H.M. Ali^{2*} and B.Y. Riad³, I.M. Ahmed²

¹Preparing and Finishing Department, National Research Centre, Cairo, Egypt.

²Chemical Engineering Department, National Research Centre, Cairo, Egypt.

³Chemistry Department, Faculty of Science, Cairo University, Egypt.

GLYCIDYL methacrylate (GMA) polymerization with waste cotton fabric by utilizing a co-initiator of ferrous cellulose thiocarbonate–hydrogen peroxide redox system was first studied under various conditions. These include the polymerization time, temperature, liquor ratio, pH and concentrations of the initiator and monomer. The product cellulose-poly(glycidyl methacrylate) graft copolymer (CPGMA) produced at best polymerization conditions was then functionalized with triethylammonium chloride (TEAC), aiming to obtain a low-cost adsorbent for dye removal from wastewater. Also, factors that affecting the amination reaction, which include; reaction time, temperature, liquor ratio, pH, and aminating agent/epoxy molar ratio were studied. The prepared amino-functionalized cellulose-poly(glycidyl methacrylate) graft copolymer (AM-CPGMA) was further characterized by the FT-IR, thermal gravimetric analysis (TGA) and surface area measurement based on Brunauer–Emmett–Teller (BET) and Barrett-Joyner-Halenda (BJH) theories. The dye adsorption capacity of the anion exchanger was also evaluated.

Keywords: Cotton fibers, Glycidyl methacrylate, Graft copolymerization, Amination.

Introduction

Various industries such as paper and pulp manufacturing, plastics, textile, leather treatment and printing consuming large amounts of synthetic chemical dyes. Annually, more than 100,000 commercial dyes exist and over 7×10^5 ton are produced worldwide [1]. Most of these dyes are un-biodegradable [2]. According to recent researches, about 12% of synthetic dyes are wasted during manufacturing and processing operations that leads to release of dyes contaminated effluents into environment [3]. Among various industries, textile industry ratings first in the consumption of dyes for coloring fiber. Dyeing industry is one of the largest water consuming industries. Discharge of dyes into water bodies maybe toxic to an aquatic life and can cause serious harm to human beings [4]. Accordingly, elimination of dyes from industrial effluents is recognized as an environmental challenge and polity legislation imposes treatment of textile wastewater. However, the treatment of dyed wastewater is very difficult because they are highly variable in composition [5], soluble in water, resistant to aerobic digestion, and are stable

to light, heat, and oxidizing agents [6]. Hence there is an endless need to have an efficient process that can remove these dyes effectively [7].

In the last years, different methods have been applied for the treatment of wastewater containing dyes such as: chemical coagulation/flocculation, chemical precipitation, electrochemical degradation [8], reverse osmosis, nano-filtration, ultra-filtration [9], electrochemical combined treatments [10], photo-catalytic degradation using UV/TiO [11], Fenton biological treatment scheme [12].

Further, amongst treatment techniques, adsorption is distinguished as a method for treating of aqueous effluent. It have several advantages like possibility of low cost regeneration, known process equipment availability, sludge-free operation and sorbets recovery [13]. Due to the various merits of activated carbon that include high surface area, micro-pore structures, high adsorption capacity and high degree of surface reactivity. It is largely used as dye adsorbent. However, commercially available activated carbon suffers of low mechanical properties, expensive and has high regeneration cost [14].

*Corresponding author e-mail: hanaamohamedaly2007@gmail.com

DOI: 10.21608/EJCHEM.2018.4885.1435

©2017 National Information and Documentation Center (NIDOC)

Because of their variety in surface and porosity, high physical-chemistry stability, regeneration and reuse for continuous process, polymeric adsorbents have been used for the removal and recovery of organic pollutants from industrial wastewater. Nevertheless, finding new adsorbents for dyes removal, with high adsorption capacities is still a challenge.

Agricultural waste-based adsorbents are a low cost, widespread, biodegradable, non-toxic, and have strong affinity for some selected dyes. However, these substances in their raw state have low efficiency, and consequently, further chemical modification by graft polymerization with vinyl monomers is an efficient method for improving the adsorption performance of a polymeric adsorbent [15].

This approach of chemical modification leads to more suitable, highly efficient, and cheap ion exchangers particularly from the agricultural waste materials. Cellulose materials are considered as good substrates for water pollutants elimination. This is based on its plenty, natural friendly polymer and its chemical and physical properties [16]. It can be manufactured in many different shapes, powders, grains, yarns, woven and non-woven fabrics. Also, different materials can be prepared from it for any kind of application. One monomer widely used is glycidyl methacrylate (GMA). It has at one end a double bond, can attach carbon centered radicals, and at the other end an epoxy group that can be utilized for further chemical modifications.

The merits of GMA over other monomers are distinguished by the fact that, it is nontoxic, uncontaminated, inexpensive, and highly reactive due to presence of epoxy group, which withdraws electron towards the second carbon atom of the double bond, and hence, facilitate its cleavage at the free radical initiation reaction. Also this group can be opened with many agents to give either anion or cation exchangers. For instance, action exchange adsorbent based on cellulosic fabric wastes carrying sulfonic acid group was synthesized by graft polymerization of glycidyl methacrylate (GMA) with consequent chemical modification of the epoxy groups with sodium sulfite/ H_2SO_4 [17]. It is demonstrated that at pH=5, the Co (II) ions ultimate adsorption capacity was 91%.

On the other hand, a cellulose-based anion exchanger was prepared through graft

copolymerization of glycidyl methacrylate onto cellulose in the presence of N, N'methylenebisacrylamide as a cross-linker followed by amination using dimethylamine and hydrochloric acid quaternization [18]. The vanadium adsorption process achieved more than 99.6% V^{5+} removal from an initial concentration of 25.0 mg/L.

The present work is concerned with the synthesis of a resin-bound quaternary ammonium salt, based on cotton waste fibers grafted with GMA monomer. Best synthesis conditions are determined, and the produced anion exchanger resin was tested with acid dye removal from synthetic solutions.

Materials and Methodology

Materials

- Waste cotton fiber was kindly supplied by Misr Spinning and Weaving Co., Mehalla El-Kubra.
- GMA (Merck) [used after purification by vacuum distillation, using rotary evaporator at 100 °C, in presence of 0.2% hydroquinone as inhibitor], sodium hydroxide (ADWIC, Egypt), sodium carbonate (ADWIC, Egypt), carbon disulfide (CS_2) (Panreac), ferrous sulfate (sd fine-chem limited), egyptol (ADWIC, Egypt), hydrogen peroxide (ADWIC, Egypt), nitric acid (ADWIC, Egypt), hydroquinone (WINLAB), acetone (ADWIC, Egypt), hydrochloric acid (sd fine-chem limited), triethylamine (ADWIC, Egypt) are used analytical grade, and C.I. Acid Black 194 (synthesia, a.s.) of commercial grade. Figure 1 represents the chemical structure of C.I. Acid black dye 194.

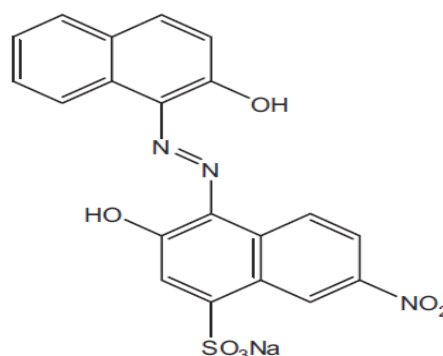


Fig. 1. Structure of C.I. Acid black dye 194.

Methodology

The adopted methodology can be described in three basic processes viz:

- Synthesis of the target product.
- Analysis and characterization.
- Testing the optimized product as dye adsorbent.

Synthesis of the anion exchange resin

Scouring [19]

Waste cotton sample was first purified by scouring in a solution containing NaOH (5gm/l), Na₂CO₃ (3gm/l) and egyptol as wetting agent (2gm/l), during 60 mins., at 90 °C within pH ranging from 12-14 and 1:40 material-to-liquor ratio, to eliminate any fatty acids or grease adhered on the cotton fibers during processing.

Thiocarbonation of Cotton sample [20]

The reaction was conducted in a 30 mL stoppered glass vessel using a thermo-controlled shaking water bath (Julabo SW21) at 30 °C constant temperature. The treated cotton sample was added to a thiocarbonation solution composed of 1%_(w/v) NaOH, 1%_(w/v) CS₂ and 0.2%_(w/v) egyptol as wetting agent to increase the reaction efficiency. The contents of the vessel, with a material to liquor ratio equivalent to 1:25, were continuously shaken throughout the thiocarbonation reaction for 2 hrs., after which, the cotton sample was pressed out using a padder. The cotton fabric in this form will be referred to as cellulose thiocarbonate.

Graft polymerization: The thiocarbonated cotton sample (0.5g) was pretreated by immersion in 0.1% ferrous sulphate solution in a 30 ml glass bottle kept at room temperature for 30 mins. After impregnation, the sample was washed, rapidly, with distilled water and pressed out until 7-8 times of its original weight. The graft copolymerization reaction was also performed in a 30 ml glass bottle, immersed into the controlled thermostatic shaking water bath, fixed at the required operating temperature (30-70 °C), where the pressed sample was mixed with the polymerization emulsion consisting of 0.2%_(w/v) egyptol (as emulsifying agent), and specific concentrations of GMA monomer and H₂O₂ (as initiator) at definite pH, with a predetermined water to material liquor ratio. After the desired reaction time (10-60 min), few drops of 250 ppm hydroquinone (in methanol) were immediately added to the reaction flask while cooling in an ice bath for terminating the polymerization reaction. The grafted product was taken out, thoroughly washed with distilled water, and then impregnated in acetone overnight,

to extract any traces of the homopolymer and the unreacted monomer that may be physically adhered to the product fibers. The final copolymer was dried at 40 °C using air dryer to a constant weight.

Aminization:

i. Preparation of triethylammonium chloride (TEAC) [21]

The preparation of the desired amine was carried out in a three neck round flask placed in an ice bath. A condenser, through which the rode of a mechanical stirrer passes for mixing the content, was mounted into the middle flask neck. The two others were connected to: - a separating funnel joined with a rubber tube expanded to the bottom of the solution and, - a pH measuring probe. A known amount of trimethylamine and approximately an equivalent amount of concentrated hydrochloric acid were charged into the flask and the funnel respectively. The acid was allowed to pass to the bottom of the flask dropwise under stirring; the final pH was around 5.

ii. Aminization procedure

1g of previously optimized Cellulose-poly(glycidyl-methacrylate) graft copolymer (CPGMA) with known epoxy content was placed in a 30 ml quick-fit glass bottle. The aqueous solution of TEAC with specified concentration and liquid to material liquor ratio is then added to the sample and the solution pH was adjusted to the desired value. The bottle with its components is then introduced into a thermostatic shaking water bath at specific temperature and the reaction is allowed to proceed for a definite time. The sample was then pressed out using the padder, washed with a dilute solution of sodium carbonate to remove any adhered amount of hydrochloric acid then washed with distilled water until filtrate neutrality and finally dried in air oven drier at 60 °C for 60 mins. The extent of aminization reactions was expressed as nitrogen percent (N%).

Analysis and characterization

Analysis: -The procedure adopted for the determination of free epoxy-ring content in the synthesized CPGMA was essentially based on Schöniger flask test [22].

-The extent of grafting with GMA is recorded by weight difference, while that of the aminization of aminated waste cotton is monitored through the nitrogen content by embracing the Kjeldahl method [23] using vapodest 20s.

-For grafting parameters determination, the

filtrates from both polymerization and extraction processes were evaporated in a known weighted round flask using a rotary vacuum evaporator at 100 °C to eliminate the solvent and any amount of the unreacted monomer, thus the following parameters could be determined:

$$\text{Polymer add-on \%} = [(w_1 - w_0) / w_0] \times 100 \quad (1)$$

$$\text{Graft yield \%} = [(w_2 - w_0) / w_0] \times 100 \quad (2)$$

$$\text{Total conversion \%} = [(w_3 - w_4) / w_3] \times 100 \quad (3)$$

$$\text{Grafting efficiency \%} = [(w_2 - w_0) / w_5] \times 100 \quad (4)$$

Where w_0 , w_1 , w_2 , w_3 and w_4 and w_5 are the weight of initial cotton sample, grafted sample without extraction, grafted sample with extraction, initial monomer charged, and total amount of grafted and homopolymer respectively.

-Finally, the aminization conversion and efficiency percent were evaluated, via:

$$\text{Aminization conversion: } [(y_0 - y_1) / y_0] \times 100 \quad (5)$$

$$\text{Aminization efficiency (mol \%): } [(y_0 - y_1) / y_2] \times 100 \quad (6)$$

Where y_0 , y_1 and y_2 are the initial amount of charged amine, un-reacted amine and epoxy content respectively.

Characterization: - Analysis by Fourier transform infra-red spectrophotometer (FT-IR) was carried out for native waste cotton, grafted cotton and aminated grafted cotton using a JASCO FT/IR6100- in the range from 400 to 4000 cm^{-1} .

- Thermal gravimetric analysis (TGA) was conducted for the three samples by thermal analyses SDTQ 600 apparatus at rate of 10 °C/min in N_2 atmosphere.

- Surface area measurements based on

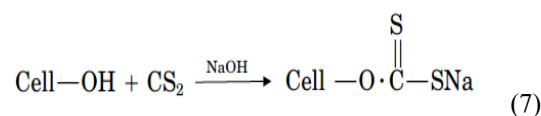
Brunauer–Emmett–Teller (BET) and Barrett–Joyner–Halenda (BJH) theories, namely, surface area (m^2/g), total pore volume (cc/g), average pore radius (nm) and the complete isotherm of native, grafted, and the aminated cotton samples were evaluated using St 2 on NOVA touch 4LX [s/n:17016062702] device.

Testing the prepared product as dye adsorbent

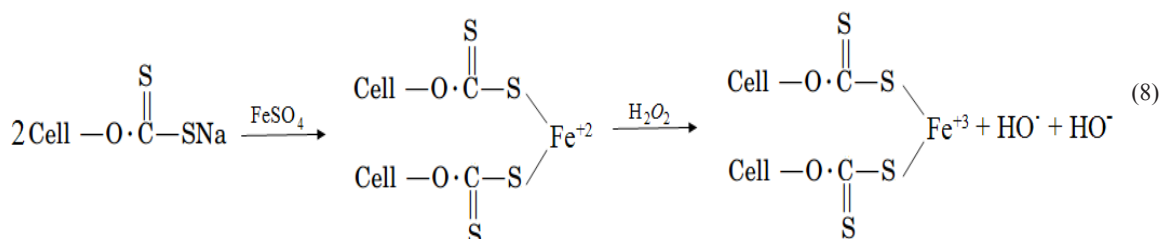
Dye sorption trial of the amino-functionalized cellulose-poly (glycidyl methacrylate) graft copolymer (AM-CPGMA), synthesized at optimum reaction conditions, was performed by immersion of 0.1g sample in 50 ml acid black dye solution of 300 ppm initial concentration. The mixture was kept at room temperature under shaking at different pH and time values. After the required time, the adsorbent sample was filtered and the filtrate was analyzed for rejected dye concentration on a Cary Series UV-Vis spectrophotometer at 575 nm maximum wavelength.

Tentative reactions mechanism

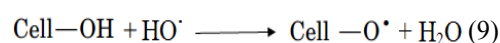
Cellulosic cotton fibers react with carbon disulphide in presence of sodium hydroxide to yield sodium cellulose thiocarbonate, according to the following equation:



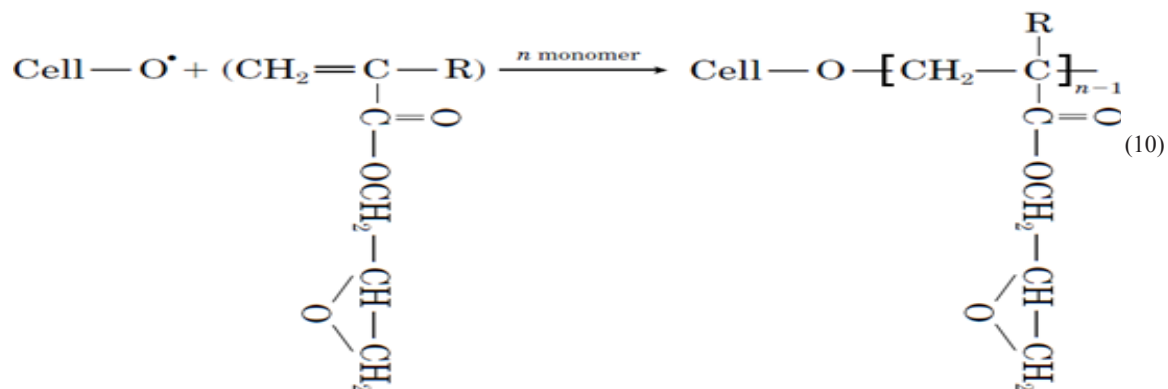
When treating the formed thiocarbonate with ferrous sulfate solution, two molecules of the former will react with one molecule of the latter forming ferrous cellulose thiocarbonate, which in turn act as a reducing agent or as a co-initiator with hydrogen peroxide to yield hydroxyl radicals (Fenton reaction), viz:



Abstraction of the hydroxyl radicals to hydrogen atoms from available hydroxyl groups of the cellulose substrate lead ultimately to cellulose macroradicals as illustrated in the following:

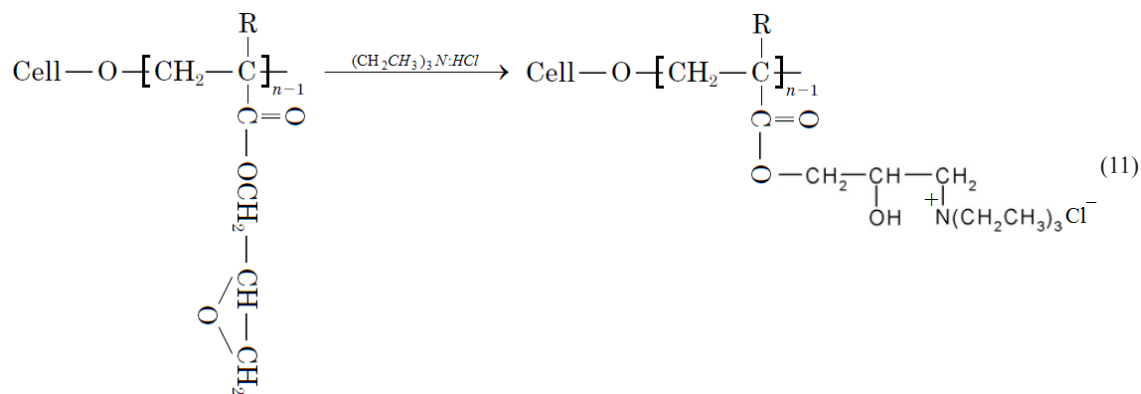


In the presence of a GMA monomer, the cellulose macroradical encourages graft polymerization of the monomer on the cellulose backbone to yield cellulose poly(glycidyl methacrylate) graft copolymer, as follows:



This copolymer (Cell-g-PGMA) can be functionalized and converted to anion exchanger by the reaction of its epoxy groups with

triethylammonium chloride to yield cationized ammonium groups with counter chlorine ions as depicted in the following reaction:



Results and Discussion

Grafting results

Effect of polymerization time

Figure 2 illustrates the dependence of the graft yield % and the epoxy content on time, by remaining constant other parameters.

As observed, the graft yield increases by increasing the polymerization time and reaches a maximum value (188%) at 30 mins. By prolonging the duration above this value, no noticeable change occurs in the graft yield, this is may be contributed to the depletion of the monomer, in addition to the reduction of active sites number on backbone of the cellulose available for the grafting as reaction proceed [17]. The graft yield % reaches to its maximum value after only 30 minutes due to the high rate and efficiency of the used ferrous cellulose thiocarbonate-hydrogen peroxide co-initiator, which in turn cease the realization of free homopolymer. Also the high conversion rate and reactivity of GMA as mentioned before was the main reason for the high rate of graft polymerization.

The epoxy content increases also by increasing the time and reaches its maximum value (1.76 mmol) after 20 mins. Afterward, it declines slightly to a constant degree as the time proceeds, probably because of conversion of certain amount of the epoxy groups formed into hydroxyl groups, since the reaction is carried out in aqueous medium and under the shown conditions, which in turn increase the reaction of epoxy groups with water or any impurities in the solution [24].

Effect of monomer concentration

A series of graft polymerization was performed in which monomer concentration was varied from 40-220%_(w/w) relative to cotton sample, while other operating conditions were held constant. As shown in Fig. 3, graft yield % increases by increasing monomer concentration in the investigated range. This is probably due to increasing the available amount of monomer at higher GMA concentrations in the vicinity of the cellulosic backbone where the latter is well known to be immovable in the reaction mixture [20].

Similarly, epoxy content increases by

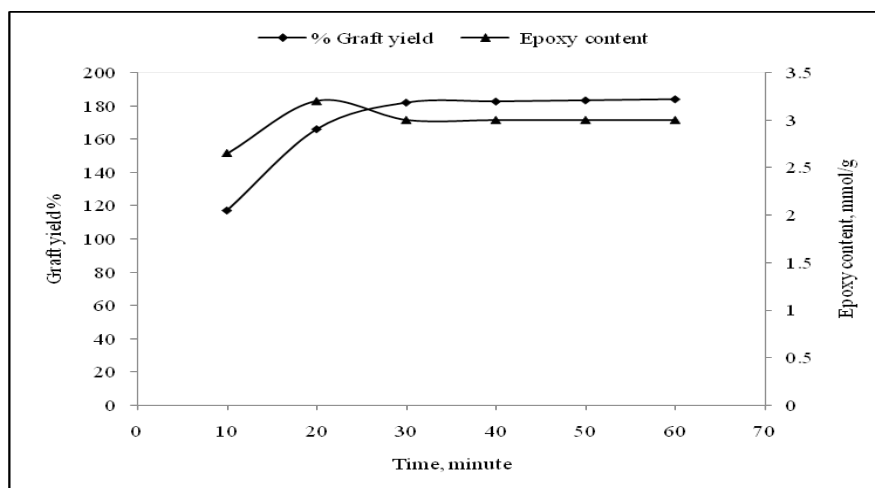


Fig. 2. Effect of time on graft yield and epoxy content, (Cotton sample 0.5g, GMA conc. 220%_(w/w) relative to sample, pH 3, H₂O₂ 0.015%_(w/v), temperature 50 °C, liquor ratio 25:1_(v/w)).

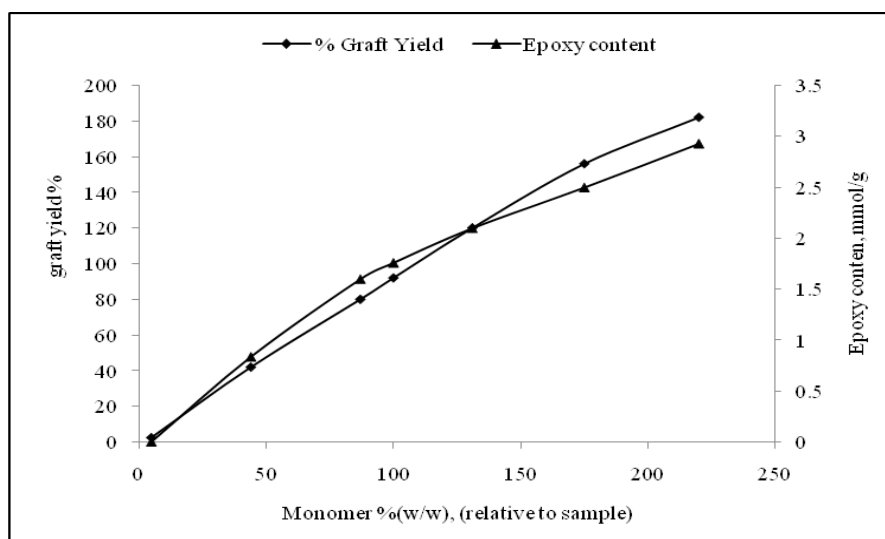


Fig. 3. Effect of monomer conc. on graft yield and epoxy content, (Cotton sample 0.5g, time 30 mins., pH 3, H₂O₂ 0.015%_(w/v), temperature 50 °C, liquor ratio 25:1_(v/w)).

increasing the monomer concentration but it is not relative to graft yield % increase, since some epoxy ring may open up during grafting as mentioned above.

Effect of pH

In this section, the reaction medium is varied by operation at variable pH values from 2-6. As illustrated in Fig. 4, the reaction occurs only in acidic medium and the graft yield % increases by decreasing the pH and reaches its maximum value

(188%) at pH 3. This is due to the fact that, the efficiency of the initiation reaction is high at low pH values due to the presence of Fe²⁺ ions, which act as co-initiator enhancing the free radical graft polymerization onto cellulose considerably. It is recognized that, at low pH values (2-4), more Fe(OH)⁺ ions is formed with higher activity than Fe²⁺ in Fenton oxidation. In contrast, at pH > 4.0, ferrous ions are unstable and can form ferric ions which have a susceptibility to produce complexes of ferric hydroxo. Further, by rising the pH value

above 9.0, these complexes can form $[\text{Fe}(\text{OH})]^{-4}$. In addition, in basic solution, H_2O_2 is unstable and may decompose to oxygen and water and lose the

ability of oxidation [25].

As shown also, the epoxy content % decreases

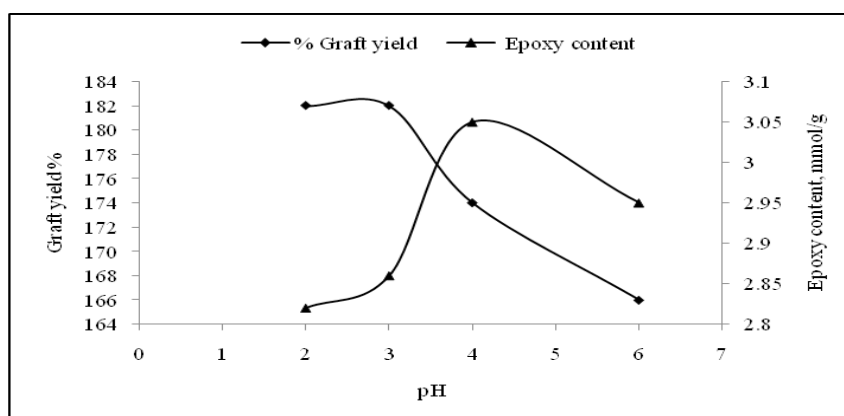


Fig. 4. Effect of pH on graft yield and epoxy content, (Cotton sample 0.5g, GMA conc. 220%_(w/w), time 30 mins., H_2O_2 0.015%_(w/v), temperature 50 °C, liquor ratio 25:1_(v/w)).

by decreasing pH, as a result of the increasing conversion of epoxy groups into hydroxyl groups by reacting with protons under the reaction conditions.

Effect of H_2O_2 concentration

As illustrated in Fig. 5, variation of H_2O_2 concentration results in a significant increase in the graft yield % up to 0.01%_(w/v), followed by a slight increase and reaches its maximum value at 0.015%_(w/v) then levels off. The regular rise at low H_2O_2 concentrations is expected due to the increase in $\cdot\text{OH}$ free radicals. The minor growth observed within 0.01%_(w/v) to 0.015%_(w/v) is may be caused by the consumption of some of the

$\cdot\text{OH}$ radicals by Fe^{2+} built in cellulose into Fe^{+3} affecting the grafting reactions. Further increase in H_2O_2 concentration results in more radicals produced, which probably combine to promote termination of the growing grafted chains. And due to the thiocarbonation step, the $\text{HO}\cdot$ are formed in the vicinity of the hydroxyl groups of cellulose chains not in the solution, this leads to the total monomer conversion is mainly grafted GMA not homopolymer and this also decreases the possibilities of termination [20].

Moreover, Fig. 4 indicates that the epoxy content increases by increasing the H_2O_2 % and reaches its maximum value at 0.015%_(w/v), and

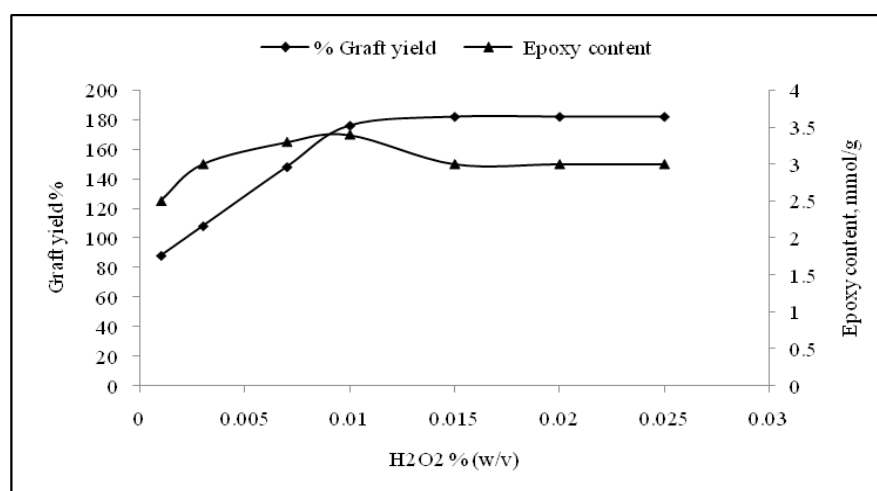


Fig. 5. Effect of H_2O_2 conc. on graft yield and epoxy content, (Cotton sample 0.5g, GMA conc. 220%_(w/w), time 30 mins., pH 3, temperature 50 °C, liquor ratio 25:1_(v/w)).

then it starts to decrease as the H_2O_2 % increases above this value, due to increasing conversion of the epoxy groups into hydroxyl groups by the increased amount of the formed $HO\cdot$ under the shown conditions.

Effect of temperature

As shown from Fig. 6, graft yield % increases by increasing the grafting temperature and reaches its maximum value at 60 °C and no noticeable change occurs in the graft yield % by increasing the temperature above this value.

This is rather a direct consequence of improvement of the solubility of the monomer and its diffusion from the solution to the fiber

and enhancement of the rate of initiation and propagation [20]. Beyond this value, raising the temperature may result in rapid termination; thereby initiate reducing the reaction rate.

In contrast, the epoxy content decreases by increasing the temperature from 30-70 °C, due to increasing the conversion of the epoxy groups into hydroxyl groups by rising the temperature above 30 °C.

Effect of liquor ratio

Figure 7 shows that the graft yield % increases with increasing the liquor ratio and attained a maximum at 1:25, where by increasing the liquor

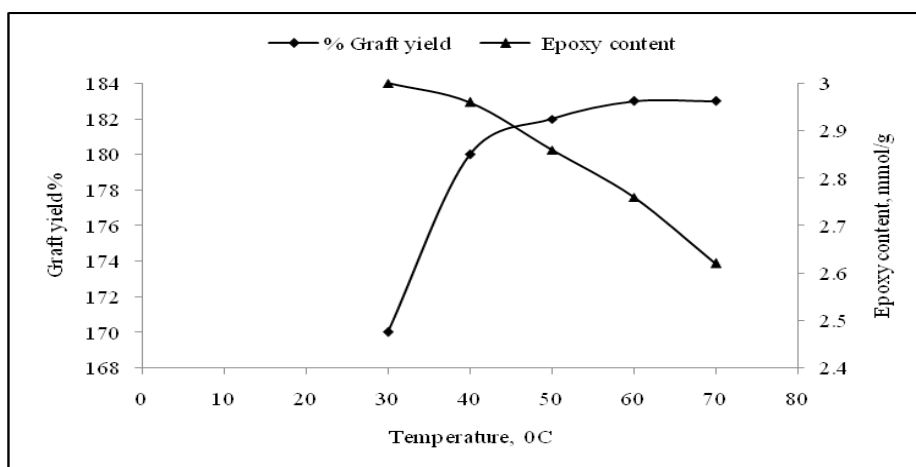


Fig. 6. Effect of temperature on graft yield and epoxy content, (Cotton sample 0.5g, GMA conc. 220%_(w/w), time 30 mins., pH 3, H_2O_2 0.015 %_(w/v), liquor ratio 25:1_(v/w)).

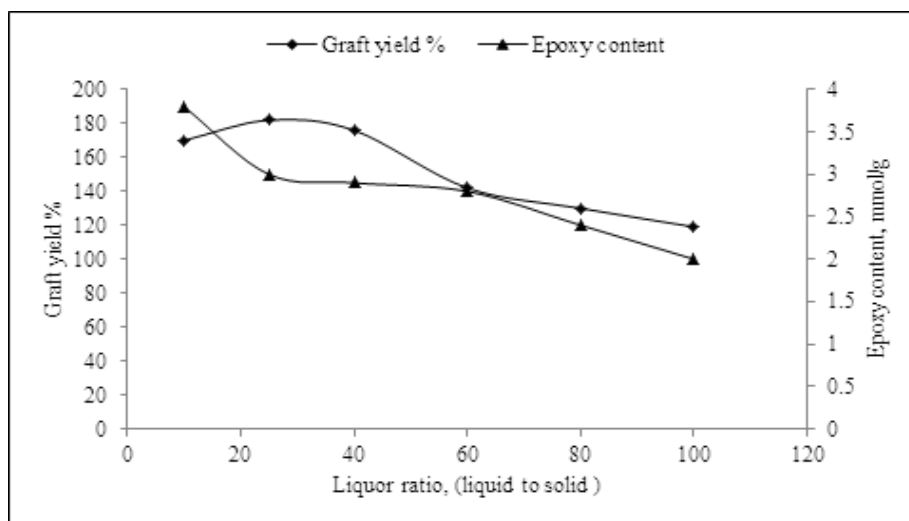


Fig. 7. Effect of liquor ratio on graft yield and epoxy content, (Cotton sample 0.5g, GMA conc. 220%_(w/w), time 30 mins., pH 3, H_2O_2 0.015 %_(w/v), temperature 50 °C).

ratio above this value, the graft yield % decreases. This can be attributed to the insufficient amount of the solvent required for transportation molecular collisions, at low material to liquor ratio. While at high material to liquor ratio, graft yield % decreases because of dilution and lower

molecular collision among the polymerization reactants [26].

Oppositely, the epoxy content is a maximum at 10:1 liquid to material liquor ratio and decreases by increasing the liquor ratio above this value.

TABLE 1. Grafting evaluation results.

Optimum grafting conditions			
GMA conc. 2220% _(w/w) , 30 mins., pH 3, H ₂ O ₂ conc. 0.015% _(w/v) , 50 °C and 1:25 liquor ratio			
Total conversion %	Grafting efficiency %	Graft yield%	Polymer add-on %
98	88	188	200

This is because of the increased conversion of epoxy groups into hydroxyl groups by increasing the amount of water under the operating conditions

Grafting evaluation results

At optimum operating conditions obtained, the evaluation of the graft polymerization process parameters results of the final graft sample was tabulated in Table 1.

Aminization results

Effect of temperature

It is noticed from Fig. 8 that, raising the reaction temperature is accompanied by a sharp

increase in the conversion of epoxy groups to amines within temperature range of 50 °C to 80 °C. This is ascribed to the satisfactory importance of temperature on:

- Copolymer swelling and enhancement of epoxy groups availabilities.
- Baeyer strain increasing in the epoxy rings, and its breaking liability increasing [27].
- Reactants kinetic energy increasing and their ability to collide.
- Supplying the system with the required energy that overcome the reaction activation energy barrier.

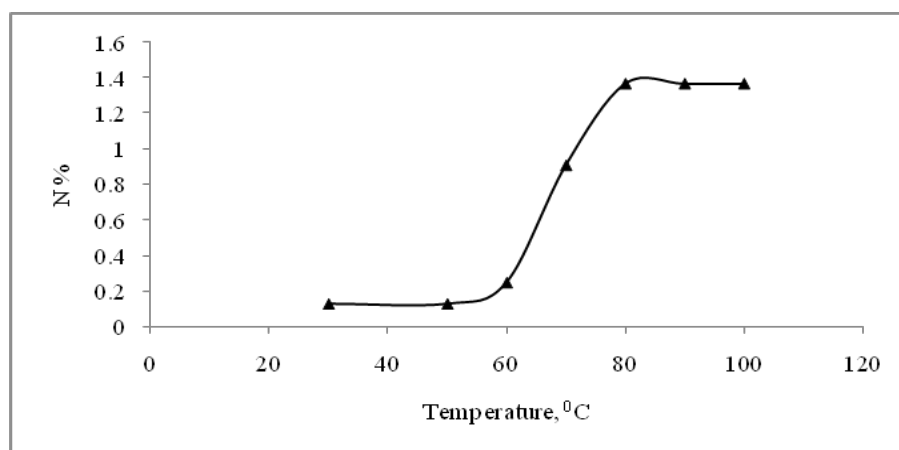


Fig. 8. Effect of temperature on % nitrogen content. CPGMA 1g (epoxy content 1.76 mmol/g), time 60 mins., pH 7, liquor ratio 12.5:1_(v/w), amine conc. 18%_(w/v).

The observed flatness over 80 °C probably indicates that both aminization and side reactions (i.e., crosslinking and hydrolysis) happen instantaneously during the operating time with nearly constant ratio. It is also noticed that by increasing the temperature from 30-50 °C, there was no change occurred in the nitrogen percent.

This may be interpreted as the extent of ring opening has a critical temperature at which the reaction proceeds rapidly.

Effect of time

Figure 9 shows that, with respect to reaction time, initially, the extent of conversion proceeds

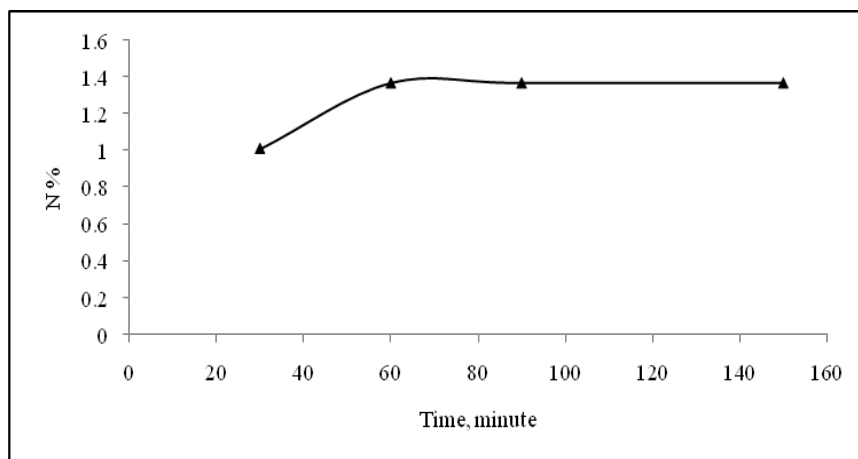


Fig. 9. Effect of time on % nitrogen content, CPGMA 1g (epoxy content 1.76 mmol/g), temperature 80 °C, pH 7, liquor ratio 12.5:1_(v/w), amine conc. 18%_(w/v).

at a fast rate up to 60 mins., between 60 and 90 mins., it decreases with time by a slower rate, then levels off over 90 mins.

This indicates that the aminization reaction ceased after 1hr and the side reactions, i.e., crosslinking and hydrolysis, predominate

thereafter [28].

Effect of pH

The initial pH was 7 and as shown from Fig. 10, the N% decreases with the decrease of pH by addition of hydrochloric acid. This may be explained as with addition of hydrochloric

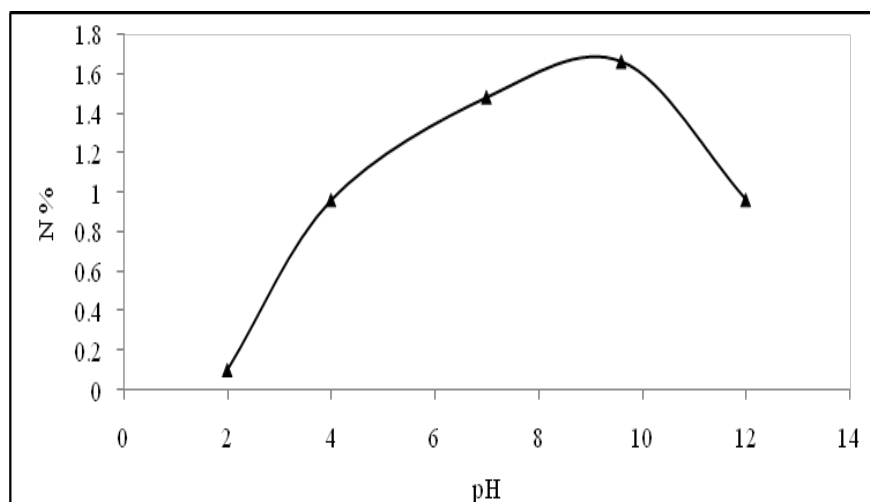


Fig. 10. Effect of pH on nitrogen content %, CPGMA 1g (epoxy content 1.76 mmol/g), temperature 80 °C, time 60 mins., liquor ratio 12.5:1_(v/w), amine conc. 18%_(w/v).

acid the reaction of Cl⁻ predominates. Increase of pH from 7 is accompanied by an increase in nitrogen percent till it attained a maximum at pH 9.6. Further increase in pH is accompanied by a decrease in the nitrogen percent. This may be due to the catalytic effect of protons on this reaction [29].

Effect of liquor ratio

Figure 11 shows that the N% was a maximum at 12.5:1 liquor ratio. There was a considerable decrease in the nitrogen percent by increasing the liquor ratio above this value. This may be due to the decrease of epoxy groups concentration on increasing the liquor ratio [30].

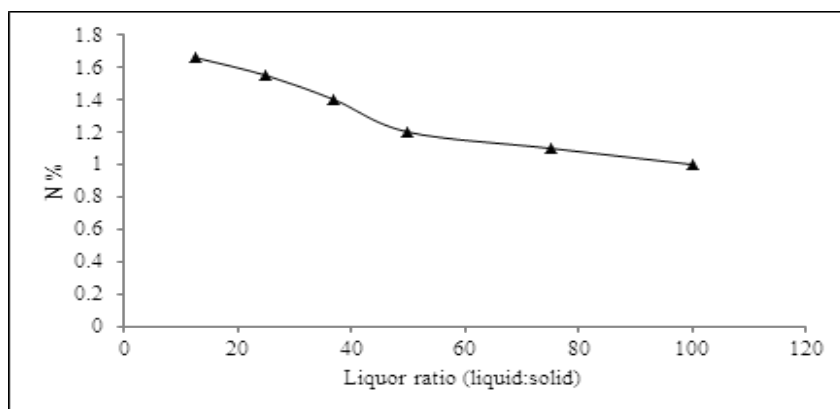


Fig. 11. Effect of liquor ratio on nitrogen content %, CPGMA 1g (epoxy content 1.76mmol/g), temperature 80 °C, time 60 mins., pH 9.6, amine conc. 18%_(w/v).

Effect of the Aminating agent/Epoxy molar ratio

Variation of the amount of amine to that of epoxy content was investigated and the results are illustrated in Fig. 12. The N% increases by increasing the aminating agent/ epoxy molar ratio up to 8:1 and then levels off. This may be explained by the consumption of most of the initial epoxy content, at low aminating agent/ epoxy molar ratios, in its reaction with water. Increasing the amine concentration is escorted by a significant

increase in the amination extents and with a slight decrease in the undesired reactions extent, i.e. hydrolysis and crosslinking. The reduction in the undesired reactions extent and increasing amine concentration may be associated with: i) amine exerted a competition to react with CPGMA, and ii) repulsive forces increasing between cellulose-poly(glycidyl methacrylate) graft copolymer (CPGMA) chains for crosslinking induced by the positive charges acquired on aminization [31].

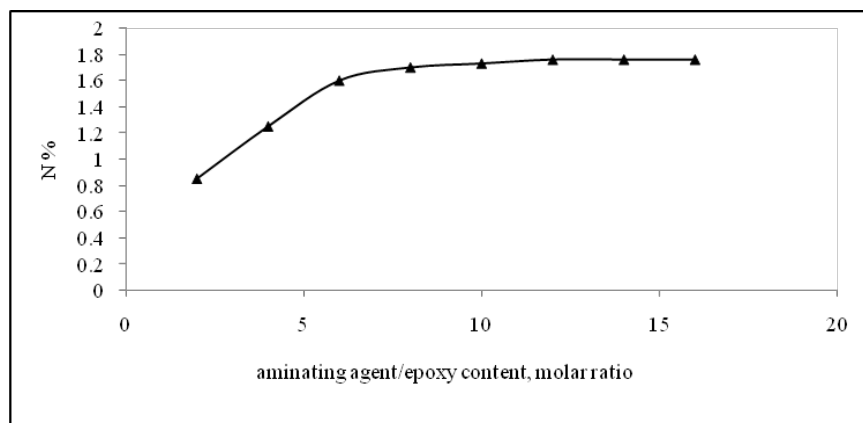


Fig. 12. Effect of amine conc. on nitrogen content %, CPGMA 1g (epoxy content 1.76 mmol/g, temperature 80 °C, time 60 mins., pH 9.6, liquor ratio 12.5:1_(v/w)).

Aminization evaluation results

At optimum conditions, the aminization parameters are determined [equations (4-5)] and the results are depicted in Table 2. The total conversion was between 8-10% and the amination % was between 83-86%. However, the total conversion % is low, the aminated sample could

be filtered and washed with distilled water only, then the nitrogen content of the produced filtrate was determined and the concentration or the molar ratio of this filtrate was adjusted to use it in another aminization reaction.

TABLE 2. Aminization evaluation results.

Optimum aminization conditions	
Aminization agent/epoxy content molar ratio 8:1, 60 mins., 80 °C, pH 10, liquor ratio 12.5:1.	
Total conversion %	Aminization efficiency %
8-10	86

*Characterization**FT-IR spectroscopy*

Figure 12 illustrates the FT-IR spectra of the native, grafted and aminated cotton. Figure 12a shows the FT-IR spectrum of the waste cotton showing a broad intense absorption band at 3428 cm^{-1} due to O-H groups. The IR spectrum of the cellulose-poly(glycidyl methacrylate) graft copolymer (CPGMA) (Fig. 12b) shows the absorption bands at 1729 cm^{-1} arising from C=O stretching vibration, also new

bands were observed at 906 , 850 and 752 cm^{-1} attributed to epoxy ring. After aminization with triethylammonium chloride, a new absorption bands at 1076 and 655 cm^{-1} (Fig. 12c) were observed which is respectively characteristic for asymmetric and symmetric stretching vibration of C-N⁺ in the quaternary ammonium group [32]. The adsorption bands characteristic for remaining epoxy ring still appears after the aminization. The existence of these characteristic bands approves the grafting of cotton with GMA and chemical

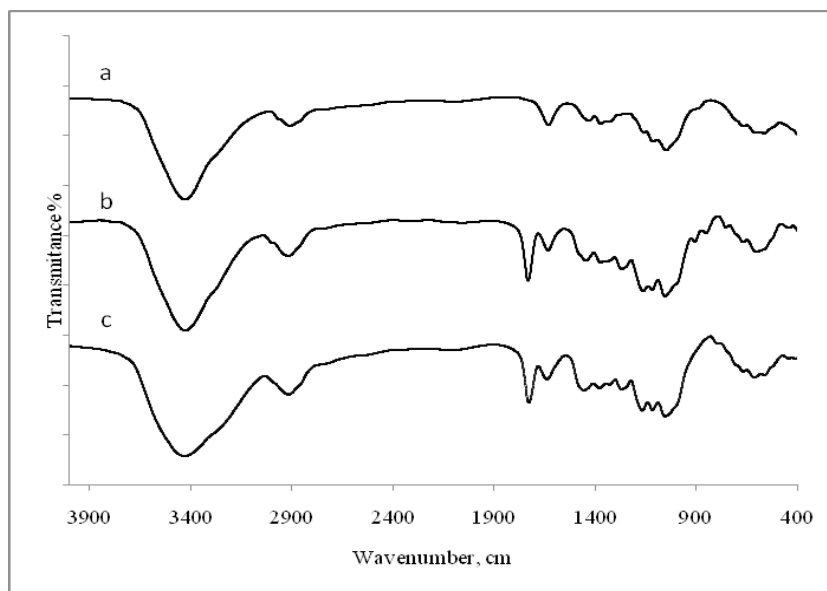


Fig. 13. FT-IR spectrum of untreated waste cotton (a), grafted cotton (b) and the aminated cotton (c).

functionalization of the GMA-grafted cotton with triethylammonium chloride.

Thermal gravimetric analysis (TGA)

4.3.2. Thermal gravimetric analysis (TGA)

Thermal stability and degree of hydrophilicity of native (Fig. 13a), grafted (Fig. 13b) and the aminated cotton (Fig. 13c) were investigated by thermal gravimetric analysis (TGA) and differential thermal gravimetric analysis (DTG). The ratio of water content in cotton fabric was 10%, which decreases to 5% after grafting,

then increases to 11% after aminization with triethylammonium chloride; this indicates that the degree of hydrophilicity decreases with grafting due to the hydrophobic nature of GMA, whereas the degree of hydrophilicity increases after aminization due to the introduction of hydrophilic amino group.

The TGA and DTG curves of native cotton are characterized by three different temperature zones. In the initial stage of decomposition (30 – 263 °C), almost 10% of the mass is lost because

of water release. In the second stage (263-393 °C), about 90% of the initial dry weight is lost as a result of the breaking of glucosidic and carbon-

carbon bonds to form a series of hydrocarbons, alcohols, aldehydes, acids, and others, followed by decomposition of these compounds into

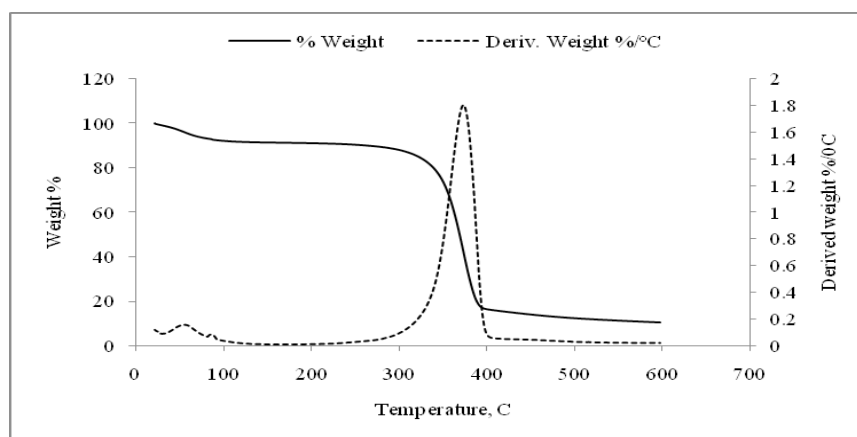


Fig. 14a. TGA curves of native cotton.

large amounts of volatiles and solid char [33]. From the derived weight calculations the highest decomposition percent in the second stage was at 370 °C.

The TGA and DTG curves of the grafted cotton show the decomposition and weight loss to occur in four different stages. In the first stage (47-202 °C) about 5% weight loss was observed,

due to water release. In the second stage of decomposition (202-265 °C) about 12% of the initial weight was lost, because of the pyrolytic of GMA polymer that was grafted onto the cellulose [33]. In the third stage (265-390 °C) the total weight loss was about 72% as a result of splitting of the cellulose structure and main-chain scission. In the final stage (390-450 °C) the total

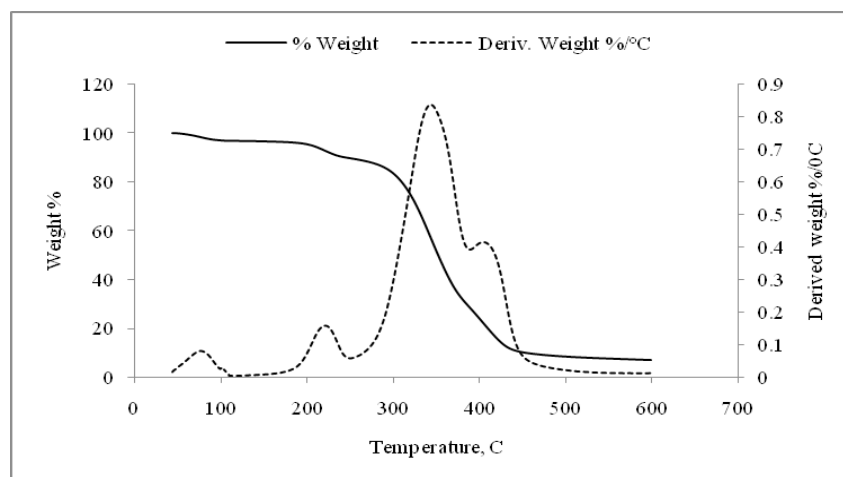


Fig. 14b. TGA curves of grafted cotton.

weight loss was about 93% due to decomposition of large amounts of volatiles and solid char. Derived weight calculations showed that the highest decomposition percent were at 214, 337 and 394 °C for the second, third and fourth stage

respectively.

The TGA and DTG curves of the aminated cotton show the decomposition and weight loss to occur in four different stages. In the first stage (42.5-210 °C) about 11% weight loss was

observed, due to water evaporation. In the second stage (210-300 °C) about 36% weight loss was detected, which may be due to the pyrolytic of GMA polymer that was grafted onto the cellulose

and removal of amino groups [17]. In the third stage of decomposition (300-390 °C) about 69% of the weight was lost, because of splitting of the cellulose structure and main-chain scission.

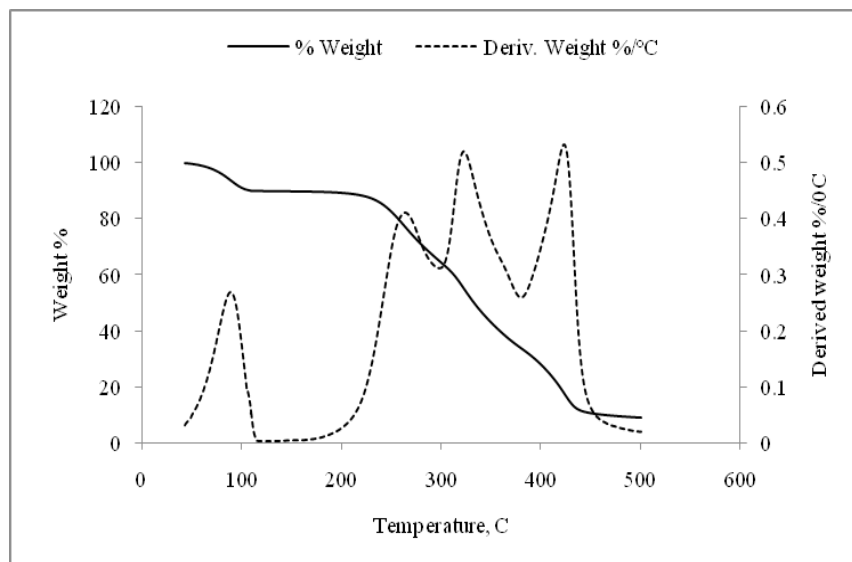


Fig. 14c. TGA curves of the aminated cotton.

In the final stage (390-450 °C) the total weight loss was about 91% because of the formation of large amounts of volatiles and solid char from the decomposed cellulose units. The highest decomposition percent were at 256.6, 318.6 and 420 °C for the second, third and fourth stage respectively.

Although amino-functionalized cellulose-poly(glycidyl methacrylate) graft copolymer (AM-CPGMA) was found to be thermally less

stable than cellulose, AM-CPGMA is stable up to 282° C, and as such, thermal stability will not pose any problems in its practical applications.

Surface area measurement (PET&BJH)

The surface area of the native and aminated cotton was measured, and the results are depicted in Table 3.

Table 3 demonstrates that the surface area and total pore volume of the native cotton increases

TABLE 3. Surface area, average pore radius and total pore volume of the native, grafted and aminated cotton.

Sample	Surface area (m ² /g)	Average pore radius (nm)	Total pore volume (cc/g)
Native cotton	20.2658	1.9236e ⁺⁰⁰⁰	1.9492e ⁻⁰⁰²
Aminated cotton	45.4314	9.5748e ⁻⁰⁰¹	2.1750e ⁻⁰⁰²

after aminization, while the average pore radius decreases. This result may be interpreted as after aminization and grinding of the aminated cotton, the surface area of cotton particles increases, these results in average pore radius decrease and total pore volume increase.

Adsorption test results

Effect of pH

As shown in Fig. 14, the pH has no effect on the adsorption capacity, q(mg/g) and the percentage removal within the whole pH range studied. The uniform sorption capacity at the equilibrium

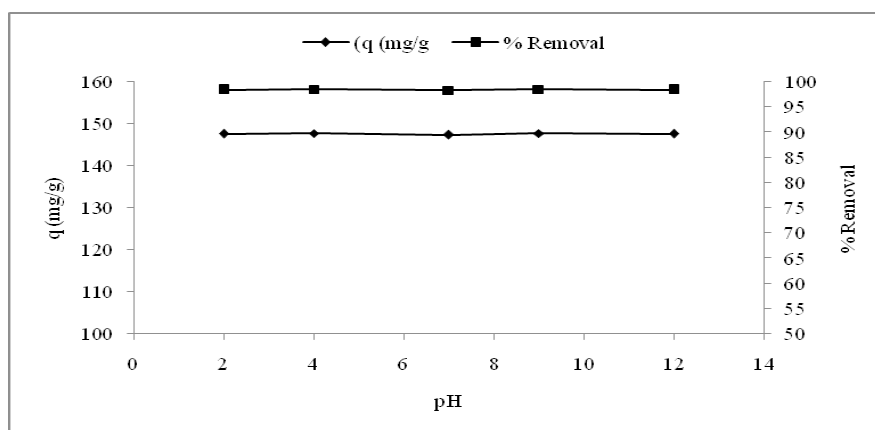


Fig. 15. Effect of pH on the adsorption and the % removal of acid black dye, (Sample 0.1g (1.7 N%), time 48 hrs., temperature 25 °C, initial dye conc. 300 ppm).

was attained because the quaternary ammonium groups are ionic in both basic and acidic medium [34, 35]. At the adsorption operating conditions stated in Fig. 14 the removal percent of the dye is almost 100% after 48 hrs.

Effect of time

Figure 15 illustrates that the adsorption capacity and the percentage removal increases as the time increase and up to approximately 30 mins. Beyond this value, it tends to level off. It

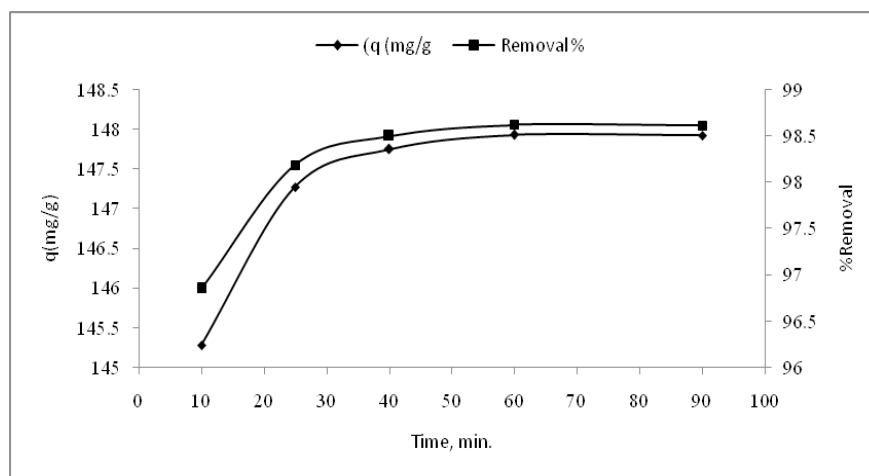


Fig. 16. Effect of time on the adsorption and the % removal of acid black dye, (Sample 0.1g (1.7 N%), pH 9, temperature 25 °C, initial dye conc. 300 ppm).

is also noticed that the adsorption capacity and the removal % have a high value approaching the maximum, and this is attributed to the high reactivity of the cationized ammonium group toward the anionic dyes [36].

Conclusion

Synthesis of the amino-functionalized cellulose-poly(glycidyl methacrylate) graft copolymer (AM-CPGMA) based on waste cotton

fibers was achieved by graft polymerization of GMA onto cotton fabric using a ferrous cellulose thiocarbonate–hydrogen peroxide redox system as a co-initiator with subsequent aminization. The best grafting results giving epoxy content equivalent to 1.76 mmol/g were at 30 mins., pH 3, H₂O₂ conc. 0.015%_(w/v), 50 °C and 25:1 liquor ratio, while the highest N% (1.76%) was at 60 mins., 80 °C, pH 9.6, 12.5:1 liquor ratio and 8:1 aminating agent/epoxy content molar ratio. The

synthesized cellulose anion exchanger (Cell-AE) was characterized by means of the FT-IR, thermal gravimetric (TGA) and surface area measurement using PET & BJH analysis. Surface area measurement indicates that the surface area (m^2/g) and total pore volume (cc/g) increased from 20.2658 and 1.9492×10^{-2} to 45.4314 and 2.1750×10^{-2} respectively with regard to native cotton and the prepared anion exchanger, and this increased the adsorption capacity. The removal of acid black dye was tested by the prepared anion exchanger and exhibited an increase from 23.83 mg/g for cotton to a maximum value of 147.27 mg/g for the prepared anion exchanger after 30 mins., at any pH value.

References

- Ibrahim, S., Fatimah, I., Ang, H.M. and Wang, S., Adsorption of anionic dyes in aqueous solution using chemically modified barley straw. *Water Sci. Technol.*, **62**, 1177–1182 (2010).
- Ayhan, D., Agricultural based activated carbons for the removal of dyes from aqueous solutions: a review. *Journal of Hazardous Materials*, **167**, 1–9 (2009).
- Aksu, Z., Application of biosorption for the removal of organic pollutants: A review. *Process Biochem.*, **40**, 997–1026 (2005).
- Shen, D., Fan, J., Zhou, W., Gao, B., Yue, Q. and Kang, Q., Adsorption kinetics and isotherm of anionic dyes onto organo-bentonite from single and multisolute systems. *J. Hazard. Mater.*, **172**, 99–107 (2009).
- Do, J.S. and Chen, M.L., Decolourization of dyecontaining solutions by electrocoagulation. *J. of Appl. Electrochemistry*, **24**, 785–790 (1990).
- El-Halwany, M., Study of adsorption isotherms and kinetic models for methylene blue adsorption on activated carbon developed from Egyptian rice hull (Part II). *Desalination*, **250**, 208–213 (2010).
- Lee, J.W., Choi S.-P., Thiruvengkatachari, R., Shim, W.-G. and Moon, H., Evaluation of the performance of adsorption and coagulation processes for the maximum removal of reactive dyes. *J. Dyes Pigment.*, **69**, 196–203 (2006).
- Fan, L., Zhou, Y., Yang, W., Chen, G. and Yang, F., Electrochemical degradation of aqueous solution of Amarnathazo dye on ACF under potentiostatic model. *Dyes Pigment*, **76**, 440–446 (2008).
- Lorenc-Grabowski, E. and Gryglewic, G., Adsorption characteristics of Congo red on coal-based mesoporous activated carbon. *Dyes Pigment*, **74**, 34–40 (2007).
- Neelavannan, M.G., Revathi, M. and Ahmed Basha, C., Photocatalytic and electro-chemical combined treatment of textile wastewater. *J Hazard Mater.*, **149**, 371–378 (2007).
- Sohrabi, M.R. and Ghavami, M., Photocatalytic degradation of Direct Red 23 dye using UV/TiO₂, Effect of operational parameters. *J Hazard Mater*, **153**, 1235–1239 (2008).
- Lodha, B. and Chaudhari, S., Optimization of Fenton biological treatment scheme for the treatment of aqueous dye solution. *J Hazard Mater.*, **148**, 459–466 (2008).
- Kapdan, I.K. and Kargi, F., Simultaneous bio degradation and adsorption of textile dye stuff in an activated sludge unit. *Process Bio Chem*, **37**, 973–981 (2002).
- Waranusantigul, P., Pokethitiyook, P., Kruatrachue, M. and Upatham, E.S., Kinetics of basic dye methylene blue biosorption by giant duck weed *Spirodela polyrrhiza*. *Environ. Poll.*, **385**, 92 (2003).
- Roy, D., Semsarilar, M., Guthriea, T.J. and Perrier, S., Cellulose modification by polymer grafting: A review. *Chem. Soc. Rev.*, **38**, 2046–2064 (2009).
- Hokkanen, S., Bhatnagar, A. and Sillanpaa, M., A review on modification methods to cellulose-based adsorbents to improve adsorption capacity. *Water Research*, **91**, 156–173 (2016).
- Sokker, H.H., Badawy S.M., Zayed, E.M., Nour Eldien, F.A. and Farag, A.M., Radiation-induced grafting of glycidyl methacrylate onto cotton fabric waste and its modification for anchoring hazardous wastes from their solutions. *Journal of Hazardous Materials*, **168**, 137–144 (2009).
- Anirudhan, T. S., Jalajamony, S. and Divya, L., Efficiency of amine-modified poly(glycidyl methacrylate)-grafted cellulose in the removal and recovery of vanadium(v) from aqueous

- solutions. *Ind. Eng. Chem. Res.*, **48**, 2118–2124 (2009).
19. Samudrika Wijayapala, U.G, Dharmasena, D.K.A.S., Bandara, D.M.N, Chathuranga, M.A.I. and Rajapakshe, K.S., Development of a new scouring methodology for the textile industry In: *National Engineering Conference, 2013, 19TH Eru Symposium, Faculty of Engineering, University of Moratuwa, Sri Lank*, 38–42 (2013).
20. Hebeish, A., Waly, A., Abdel-Mohdy, F. A. and Aly, A. S., synthesis and characterization of cellulose ion exchangers. i. polymerization of glycidyl methacrylate, dimethylaminoethyl methacrylate, and acrylic acid with cotton cellulose using thiocarbonate–H₂O₂ redox system. *Journal of Applied Polymer Science*, **66**, 1029–1037 (1997).
21. Harland, C.E., *Ion Exchange. Theory and Practice*. The Royal Society of Chemistry, Cambridge (1994).
22. Abou-Zeid, N. Y., Waly, A., El-Alfy, E. A. and Hebeish, A., Fe⁺²-thiourea dioxide-H₂O₂ induced polymerization of glycidyl methacrylate and its mixtures with acrylamide, acrylonitrile, butylmethacrylate, or styrene with cotton fabric. *Journal Of Applied Polymer Science*, **27**, 2105–2117 (1982).
23. Cole, J.O., Parks, C.R., A semimicro-kjeldahl distillation apparatus, *Ind. Eng. Chem. Anal. Ed.*, **18** (1), 1–82 (1946).
24. Bonollo, S., Lanari, D. and Vaccaro, L., Ring-opening of epoxides in water. *Eur. J. Org. Chem.*, 2587–2598 (2011).
25. Shaobin Wang., A Comparative study of Fenton and Fenton-like reaction kinetics in decolourisation of wastewater. *Dyes and Pigments*, **76**, 714–720 (2008).
26. Shakila, P., Rekha, K.R., Vijayalakshmi K. and Sudh, P. N., Synthesis, characterization and optimisation of carboxymethyl chitosan graft glycidyl methacrylate copolymer. *International Journal of Applied and Advanced Scientific Research*, **1**(2), 2456–3080 (2016).
27. Reutov, O., *Theoretical Principles of Organic Chemistry*, Ed. Engl., Chap. 4, Mir, Moscow, p. 242 (1967).
28. Kubota, H. and Ujita, S., Reactivity of glycidyl-methacrylate-grafted cellulose prepared by means of photografting. *Journal of Applied Polymer Science*, **56**, 25–31(1995).
29. Mika, T. F., In *Epoxy Resins, Chemistry and Technology*, Eds., C. A. May, Y. Tanaka, Chap. 4, Dekker, New York, 239 (1973).
30. Abou-Shosha, M.H. and Ibrahim, N.A., Reaction of cellulose-poly(glycidyl methacrylate) with methylamine. *Die Angewandte Makromolekulare Chemie*, **152**, 93–106(1987).
31. Khalil, M. I., Wally, A., Kantouch, A., Abo-Shosha, M. H., Preparation of ion-exchange celluloses. I. Anion exchange celluloses, *Journal of Applied Polymer Science*, **38**, 313–322 (1989).
32. Migahed, M.A., Shabana, M.M., Fadda, A.A., Tamer, A.A. and Negm, N. A., Synthesis of some quaternary ammonium gemini surfactants and evaluation of their performance as corrosion inhibitors for carbon steel in oil well formation water containing sulfide ions. *The Royal Society of Chemistry Advances*, **5**, 104480–104492 (2015).
33. Donia, A.M., Atia, A.A., El-Boraey, H. and Mabrouk, D.H., Uptake studies of copper(ii) on glycidyl methacrylate chelating resin containing Fe₂O₃ particles. *Sep. Purif. Technol.*, **49**, 64–70 (2006).
34. Wawrzkiwicz, M. and Hubicki, Z., *Ion Exchange - Studies and Applications*, 61–63 (2015).
35. Constantina, M., Asmarandeia, I., Harabagiua, V., Ghimicia, L., Ascenzib, P., and Fundueanua, G., Removal of anionic dyes from aqueous solutions by an ion-exchanger based on pullulanmicrospheres. *Carbohydrate Polymers*, **9**, 74– 84 (2013).
36. Liu, L., Gao, Z., Su, X., Chen, X., Jiang, L., and Yao, J., Adsorption Removal of Dyes from Single and Binary Solutions Using a Cellulose-based Bioadsorbent. *ACS Sustainable Chem. Eng.*, **3**(3), 432–442 (2015).

(Received 26/8/2018;

accepted 3/10/2018)

تحضير وتوصيف مبادل ايوني مبني على عوادم الاليف القطنية لإزالة الصبغات من المخلفات السائلة

أحمد إبراهيم والي^١، معالي عبد المنعم خضر^٢، هناء محمد علي^٢، بهيه يحيى رياض^٢، اسلام محمد احمد^٢
^١قسم التحضيرات والتجهيزات - المركز القومي للبحوث - القاهرة - مصر.
^٢قسم الهندسة الكيميائية - المركز القومي للبحوث - القاهرة - مصر.
^٣قسم الكيمياء - كلية العلوم - جامعة القاهرة - مصر.

طبقا للدراسات الحديثه ١٢٪ تقريبا من الصبغات المحضره صناعيا تفقد اثناء عمليات التحضير والتطبيق، ٢٠٪ تقريبا من هذه الصبغات المفقوده تنتقل لمياه الصرف الصناعي.

تمثل هذه الصبغات خطر كبير على الكائنات الحيه، لذا فقد تم تطوير العديد من الطرق لازالتها من المخلفات السائله. ولكن معظم هذه الطرق ذات تكلفه عاليه وكفاءه منخفضه بالا اضافه الى ان بعضا من هذه الطرق قد ينتج بدوره مواد ضاره بالبيئه والكائنات الحيه. من بين هذه الطرق المستخدمه لازالة الصبغات من المخلفات السائله هي طريقه التبادل الايوني باستخدام مبادلات ايونيه محضره عن طريق البلمره التطعيميه لبعض المونمرات على اسطح بعض البلمرات الطبيعيه التي تمتاز بكونها متوفره، امنه على البيئه، قابله للتحلل ورخيصه الثمن.

نتيجة لما سبق ففي العمل الحالي تم تحضير مبادل ايوني عن طريق البلمره التطعيميه لاحد المونمرات (glycidyl methacrylate) مع العوادم القطنيه الناتجه اثناء مراحل صناعة النسيج المختلفه ثم تفعيله بادخال أحد مجموعات الأمين.

تم دراسة تأثير العوامل المختلفه للتفاعل مثل تركيز المواد المتفاعله، الزمن، الحراره، الاس الهيدروجيني ونسبه المواد السائله للمواد الصلبه على خواص المبادل الايوني الناتج وكذلك تأثير هذه العوامل على كفاءته في ازالة الصبغات.

تم توصيف المنتج بالطرق الكيميائيه مثل تحديد محتوى مجموعات الالبوكسي والمحتوى النيتروجيني والطرق الفزيائيه مثل الاشعه تحت حمراء والتحليل الحراري وقياس المساحة الكليه للسطح.